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**MODELLING OF DECENTRAL DHW PREPARATION IN LARGE  
MULTI-FAMILY BUILDINGS**

CANDIDATO

Stefano Fisco

RELATORE

Chiar.mo Prof. Ing. Gian Luca Morini

CORRELATORI

Dr.-Ing. Fabian Ochs

Dr.-Ing. Georgios Dermentzis

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# List of symbols and abbreviations

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|                |   |
|----------------|---|
| $C_{HX}$       | Thermal capacity of the heat exchanger [J/K]                                      |
| $c_p$          | Specific heat [J/kgK]   |
| DHHX           | District heating heat exchanger   |
| DHW            | Domestic hot water  |
| E              | Energy [J]  |
| fdiv           | Control signal of the mixer-diverter  |
| FE             | Final Energy  |
| fs             | Smultaneity factor  |
| FWS            | Fresh water station   |
| HP             | Heat pump   |
| HP             | Heat pump   |
| HX             | Heat exchanger  |
| iPHA           | International passive haus association  |
| m              | Mass [kg]   |
| $\dot{m}$      | Mass flow [kg/s]  |
| PHPP           | Passive House Planning Package  |
| Q              | Energy [J]  |
| s              | Thickness [mm]  |
| S              | Surface [m <sup>2</sup> ]   |
| $T_{bot}$      | Bottom temperature of the storage [°C]  |
| $T_{top}$      | Top temperature of the storage [°C]   |
| $U_{AHL}$      | Heat transfer coefficient to ambient [W/K]  |
| $U_{AHX}$      | Heat transfer coefficient between primary and secondary side heat exchanger [W/K] |
| UE             | Useful energy   |
| V              | Volume [m <sup>3</sup> ]  |
| $\Delta\theta$ | Temperature difference [K]  |
| $\theta$       | Temperature [°C]  |
| $\lambda$      | Termal conductivity [W/(m·K)]   |
| $\rho$         | Density [kg/m <sup>3</sup> ]  |
| $\Psi$         | Dimensionless temperature change  |

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# Extended abstract

This master thesis contributes to the need to design more efficient heating and domestic hot water preparation systems to support the ambitious need of limiting the CO<sub>2</sub> emissions in accordance to the European goals. While for heating good solutions were developed within the last decades, there is still a need for improving domestic hot water (DHW) preparation and supply systems, which represent, nowadays, a considerable percentage of the total energy expense in households, especially in good energy performance buildings such as Passive Houses.

In this context, dynamic building and simulation plays an important role in the development of DHW preparation systems for residential buildings, in order to evaluate and optimize the final energy and the DHW comfort (evaluated as temperature of the DHW supplied to the user and the so-called “waiting time” to reach the set point of this temperature).

The case study of this work is a big multi-family building composed of 96 flats that will be built in the neighbourhood “Campagne” in Innsbruck.

A fresh water station (FWS) is placed in each flat for the DHW preparation. FWS is a unit for the decentral, i.e. flat-wise instant DHW preparation, and it is composed by one heat exchanger (HX), and the control systems implemented in order to respond to the user requests and assure the working conditions of the HX. In this specific case study, district heating (DH) is used to heat up the water in the storage tank located in the technical room of the building. A distribution system connects the storage to all the FWS in the flats.

Energy and comfort evaluations are strongly influenced by the DHW profiles. For the flat-level simulations, these profiles can be either derived from standard profiles, e.g. EN16147 (here, profile M) or from stochastic tools, e.g. such as DHWcalc, which creates a DHW profile using a stochastic approach (flat-level and building level DHW profiles).

The physical approach for the simulation of DHW preparation on building-level is to simulate the whole building with one HX in each flat: for big multi-family buildings, this approach would lead to a very heavy model and extensive simulation times. The second approach is to simulate the DHW preparation on flat-level and then extrapolate the results to the whole building: however, this method significantly overestimates the required heating power. The third approach is to simulate the building-level DHW preparation with a single HX which approximates the behaviour of all the HXs of the building. For this purpose, the simultaneity factor ( $f_s$ ) should be considered (i.e the simultaneity of DHW use). For the building-level DHW

preparation, in fact, it is important to consider that only a limited number of flats will consume the DHW at the same time and so that the building peak loads cannot be evaluated as the sum of the peak loads of each flat. In the framework of this thesis, the third approach is chosen as the most appropriate for the simulations. However, in order to prove the reliability of the approach, this approach is compared to the physical approach, using a small multi-family building composed of 10 flats.

In order to parametrize the HX for the whole building, a DHW profile for the building should be derived (building-level DHW profile). The DHW profile for a building is implemented through the generalization of the profiles derived for the flat. Four different DHW profiles for the building are implemented: 1) hourly average profile (i.e. the tappings derived from standard EN16147, profile M, averaged to hourly time steps); 2) 10 seconds profile (i.e. a profile derived from EN16147 where the daily tapping cycle of each flat occurs with a delay of 10 seconds for each flat); 3) 39 seconds profile (same profile as the second one but with a delay of 39 seconds for each flat); 4) stochastic profile (i.e. a profile derived from *DHWcalc* which distributes the daily tapping all over one day, setting reference conditions such as volume of DHW daily required and duration of the tappings).

First, a representative model of the FWS for each flat is implemented in Matlab/Simulink simulation environment, considering a 35 kW HX (which corresponds to a HX of a typical market available FWS). The two flat-level profiles are tested on this model together with two different control strategies of the circulation pump, showing that the control strategy influences how the set point temperature of the DHW supplied to the user is achieved (useful energy and waiting time).

From the flat-level model, a building-level model is derived. The four different building-level profiles are used to evaluate the simultaneity factor, and so the peak load of the building, in order to size the HX for the whole building. For each profile three main parameters of the heat exchanger are calculated: heat transfer coefficient between primary and secondary side ( $UA_{HX}$ ), heat transfer coefficient to the ambient ( $UA_{HL}$ ) and thermal capacity ( $C_{HX}$ ).

The DHW profiles (and so the simultaneity factor  $f_s$ ) and the parametrization of the HX influence the results. Final energy and DHW comfort (i.e. the DHW temperature and the “waiting time” to reach this temperature) are compared in each case. The return temperature of the fluid sent back to the storage is also analysed. The development of the return temperature to the storage is influenced by the DHW profiles and the thermal capacity of the pipe. The return temperature to the storage has similar developments for all the analysed DHW profiles,



except for the *10s profile* which is the one with the highest *fs*. With this profile, the return temperature to the storage is higher in the period between 13:00 and 22:00. For this reason, the thermal losses observed with the *10s profile* are higher if compared to the other cases.

In future works the influence of the insulation of the pipe on the return temperature to the storage (and so on the thermal losses) should be evaluated. Future studies should also investigate the influence on the results of different boundary conditions and DHW system design.

# Extended abstract

Il lavoro svolto contestualmente a questa tesi risponde all'esigenza di progettare efficienti sistemi di riscaldamento e produzione di acqua calda sanitaria (ACS), seguendo gli ambiziosi obiettivi europei in materia di riduzione delle emissioni di CO<sub>2</sub>. Per i sistemi di riscaldamento sono state sviluppate ottime soluzioni nell'arco degli ultimi anni, ma importanti sforzi sono ancora da compiere per ottimizzare i sistemi di produzione e distribuzione di ACS che rappresentano, ad oggi, una percentuale considerevole della spesa energetica nelle abitazioni (specialmente in edifici con buone prestazioni energetiche, come le Passive Houses).

In questo contesto, la simulazione dinamica degli edifici gioca un ruolo fondamentale nello sviluppo di sistemi di produzione di ACS per edifici residenziali, permettendo di valutare ed ottimizzare il consumo di energia e il comfort (valutato rispetto alla temperatura dell'ACS fornita all'utente e il cosiddetto "waiting time", ovvero il tempo necessario per il raggiungimento del set point di questa temperatura).

Il caso studio di questo lavoro è un grande edificio multi-familiare, composto da 96 appartamenti, che verrà costruito nel quartiere "Campagne", nella città di Innsbruck.

Una fresh water station (FWS) è collocata in ciascun appartamento ed è utilizzata per la produzione di ACS. Una FWS è un'unità decentrata per la produzione istantanea di ACS nell'appartamento, ed è composta da uno scambiatore di calore (HX) e dai sistemi di controllo che permettono di rispondere prontamente alle richieste dell'utenza, assicurando le condizioni di funzionamento dell'HX. In questo specifico caso studio, la connessione ad una rete di teleriscaldamento (DH) è utilizzata per riscaldare l'acqua presente all'interno di un serbatoio di stoccaggio termico, posizionato nel locale tecnico dell'edificio. Un sistema di distribuzione collega il serbatoio a tutte le FWS negli appartamenti.

Le valutazioni energetiche e sul comfort sono fortemente influenzate dai profili d'uso dell'utenza (DHW profiles). Per la simulazione di un unico appartamento (flat-level), il profilo d'uso può essere ricavato da un profilo standard, ad esempio EN16147 (profilo M, nel caso di questo lavoro) o da appositi tools, ad esempio DHWcalc, che permette di creare un profilo d'uso seguendo un approccio stocastico.

L'approccio fisico per simulare la produzione di ACS per l'intero edificio (building-level), prevede la simulazione dell'intero edificio con un HX in ciascuno degli appartamenti: per grandi edifici multi familiari, questo approccio richiederebbe l'implementazione di un modello troppo pesante, nonché tempi di simulazione eccessivi. Il secondo approccio simula la

produzione di ACS per un singolo appartamento, per poi estrapolare i risultati all'intero edificio: questo metodo tende a sovrastimare la potenza richiesta per la produzione dell'ACS. Il terzo approccio simula la produzione di ACS per l'intero edificio, tramite un singolo HX che approssima il comportamento di tutti gli HXs dell'edificio. Per poter dimensionare questo HX, è necessario tenere in considerazione l'effetto del simultaneity factor  $f_s$  (ovvero il fattore di simultaneità dell'uso di ACS nell'edificio). Per la produzione di ACS per l'intero edificio, infatti, è importante considerare che solo un limitato numero di appartamenti richiederà ACS nello stesso momento e quindi il carico di picco dell'edificio non può essere valutato come la somma dei carichi di picco di ciascun appartamento. Nell'ambito di questa tesi, è stato scelto il terzo approccio come il più appropriato per le simulazioni. Tuttavia, per esaminare l'affidabilità di questo approccio, lo stesso è stato confrontato con l'approccio fisico, usando un edificio multi familiare più piccolo, composto da 10 appartamenti.

Al fine di parametrizzare l'HX per l'intero edificio, è necessario ricavare un profilo d'uso di ACS dell'intero edificio. Il profilo d'uso di ACS per l'intero edificio è implementato attraverso la generalizzazione dei profili d'uso ricavati per un appartamento. Sono stati implementati quattro diversi profili d'uso di ACS dell'edificio: 1) profilo orario medio (i.e. i prelievi d'acqua ricavati dal profilo standard EN16147, sono stati mediati su un time step di un'ora); 2) profilo ogni 10 secondi (i.e. un profilo derivato da EN16146 in cui il ciclo giornaliero di prelievi d'acqua per ciascun appartamento inizia con un ritardo di 10 secondi); 3) profilo ogni 39 secondi (stesso profilo del secondo caso ma con un ritardo di 39 secondi per ciascun appartamento); 4) profilo stocastico (i.e. un profilo derivato dal DHWcalc che distribuisce i prelievi giornalieri lungo l'arco di una giornata, sulla base di input come il volume di ACS richiesto in un giorno e la durata dei prelievi di ACS).

Per primo è stato sviluppato e dimensionato un modello rappresentativo della FWS di ciascun appartamento, nell'ambiente di simulazione Matlab/Simulink, considerando un HX di 35 KW (corrispondente alla taglia di un HX di una tipica FWS disponibile in commercio). Su questo modello sono stati testati i due diversi profili d'uso di un appartamento e due diverse strategie di controllo della pompa di circolazione, mostrando le modalità con cui la strategia di controllo influenza il raggiungimento della temperatura di set point dell'ACS fornita all'utenza (energia utile e *waiting time*).

Dal modello della FWS dell'appartamento è stato ricavato un modello di FWS per l'intero edificio. I quattro diversi profili d'uso dell'edificio sono utilizzati per valutare il simultaneity factor, e quindi il carico di picco, in modo da poter dimensionare l'HX per l'intero edificio. Per

ciascun profilo sono stati calcolati tre diversi parametri dell'HX: coefficiente di scambio termico tra il circuito primario e secondario ( $UA_{HX}$ ), coefficiente di scambio termico con l'ambiente ( $UA_{HL}$ ) e capacità termica ( $C_{HX}$ ).

Il profilo d'uso di ACS (e quindi il simultaneity factor) e la parametrizzazione dell'HX influenzano i risultati. L'energia per la produzione di ACS e il comfort termico (i.e. temperatura dell'ACS e “*waiting time*” per raggiungere questa temperatura) sono confrontati nei diversi casi. Anche l'andamento della temperatura di ritorno dell'acqua al serbatoio di stoccaggio termico è analizzata. L'andamento di questa temperatura è influenzato dal profilo d'uso di ACS e dalla capacità termica dei tubi. La temperatura di ritorno al serbatoio di stoccaggio termico ha un andamento simile per ciascuno dei casi analizzati con i diversi profili d'uso, tranne che per il caso denominato *profilo ogni 10 secondi*, che è il profilo con il più alto valore del simultaneity factor. Nel periodo tra le 13:00 e le 22:00, infatti, con questo profilo d'uso, si osserva che il valore della temperatura di ritorno al serbatoio è più alto rispetto agli altri casi.

In sviluppi futuri dello studio, verrà valutata l'influenza dell'isolamento termico sulla temperatura di ritorno al serbatoio termico. Studi futuri, inoltre, indagheranno l'influenza sui risultati di diverse condizioni al contorno e di diversi design del sistema di produzione di ACS.

# Chapter 1. Introduction

## 1.1. Motivation of the work

Residential buildings are known to strongly influence energy consumption. In developed countries, up to 40% of total energy consumption is spent in residential sector, exceeding industrial and transportation sectors (Perez-Lombard, Ortiz, & Pout, 2007). Deep studies on how to reduce this expense are always in the spotlight in the scientific field.

Many of the studies found in literature are focused on how to improve simulation studies in order to optimize energy consumption of the buildings (Dermentzis, et al., 2017); (Dermentzis, et al., 2019). These studies, focused on dynamic simulation methods, aim to reduce the amount of energy consumption imputable to heating systems.

The energy consumption for DHW (Domestic Hot Water) preparation still remains a not-deeply studied topic in dynamic simulation. DHW usage per person can be 30% higher than the values assumed in planning tool like PHPP (Clarke & Grant, 2010).

A residential district will be built in Innsbruck (Austria) and its energetic optimization is the core of the so-called Campagne research project, which aims to minimize the environmental impact of a multi-family building district. Previous studies have already compared different heating generation systems (Dermentzis, 2019). The aim of this work, instead, is to deeply investigate the modelling DHW preparation for big multi-family buildings, excluding space heating. The considered reference building is a 96-flat building.

A model for DHW preparation is implemented for a single flat (flat-level DHW preparation). In order to simulate the DHW preparation for the whole building, this model can be used for each of the flats. This approach is used for small multi-family building (10-flat building). However, for a big multi-family building it would be hard to implement and it would be time and computational consuming. Thus, an alternative method to simulate the DHW preparation for the whole building (building-level DHW preparation) is developed with a central HX that covers the request of the whole building.

In the proposed method, the parametrization of the HX is crucial. The parameters of the HX are assumed in order to approximate the behaviour of all the HXs of the building together.

The length and the diameter of the pipes strongly influences the heat losses (van der Heijde, Aertgeerts, & Helsen, 2017). In reality, a pipe system connects the central storage tank with

each flat of the building. The length of the pipe between the storage tank and the central HX, for the building-level model, is then assumed as the total length of the pipe system in reality. The thermal losses resulting from the simulation are influenced by this assumption. This approximation also highlights the influence of the thermal capacity of the pipes in the determination of the temperature of the water circulating in it.

Different DHW user profiles are tested in order to check their influence on the simulation results. In view of the importance of the profiles on such a study, a DHW consumption profile for the building should be derived. Anna Marszal-Pomianowska presents a method to calculate mean hourly and daily usage profile of DHW extrapolating values from hourly data of entire year, explaining that, the sizing of the hydraulic systems benefits if it is based on accurate information on the profile (Marszal-Pomianowska, et al., 2019). Based on measured data several methods can be used to predict a building profile (de Santiago, Rodriguez-Villalón, & Sicre, 2017); (Ahmed, Pylsy, & Kurnitski, 2016). When no measured data are available, a set of information can still be collected to predict a stochastic profile with the method proposed by Ulrike Jordan (Jordan & Vajen, 2001) who also developed a tool called DHWcalc ("DHWcalc, Tool for the Generation of Domestic Hot Water (DHW) Profiles on a Statistical Basis"), which allows to generate stochastic profiles. Building usage profiles can also be derived from EN16147, which presents a daily tapping cycle for a single-family apartment occupied by 4 people (EN16147, 2017).

In this work, two DHW profiles are used: one derived from the EN16147 profile M and one created with DHWcalc. In the flat-level DHW preparation, both profiles are tested and compared. In Building-level DHW preparation, three profiles derived from the standard EN16147 and one stochastic profile created with DHWcalc are tested and compared.

The reliability of the method is then tested on a small multi-family building on the basis of the work by Samuel Breuss. A small multi-family building of 10 flats is considered. Two different models are developed and analysed: the first model, develops the building-level approach considering a central HX while the second model, considers each flat with its own HX.

This work contributes to the literature by proposing and testing a method to simulate DHW production in big multi-family buildings. All the HXs of the building are modelled as one HX. The method suggests how to choose geometric size, power and thermal capacity of the central HX. The capacity of the HX is varied in different simulations, based on the  $f_s$  in order to approximate a realistic behaviour of 96 HXs together. The aim is to derive energy and comfort

evaluation for DHW preparation with the implemented method, showing how the DHW profile influences the results.

## 1.2. Overview of the project

A new residential district will be built in Innsbruck (Austria). The total area occupied by the district is around 84000 m<sup>2</sup> and it includes 16 buildings grouped in 4 blocks (see Figure 1). The total number of flats is 1128 and the district also includes sport facilities, green areas and social infrastructures. Each block consists of four buildings (see Figure 2) with an average of 71 apartments per building. The research project Campagne is mainly focused on the energetic optimization of the residential part and each building is projected to be built according to Passive House standards (iPHA).

The reference building of this work is Building A in Block 1, which is represented in Figure 3.

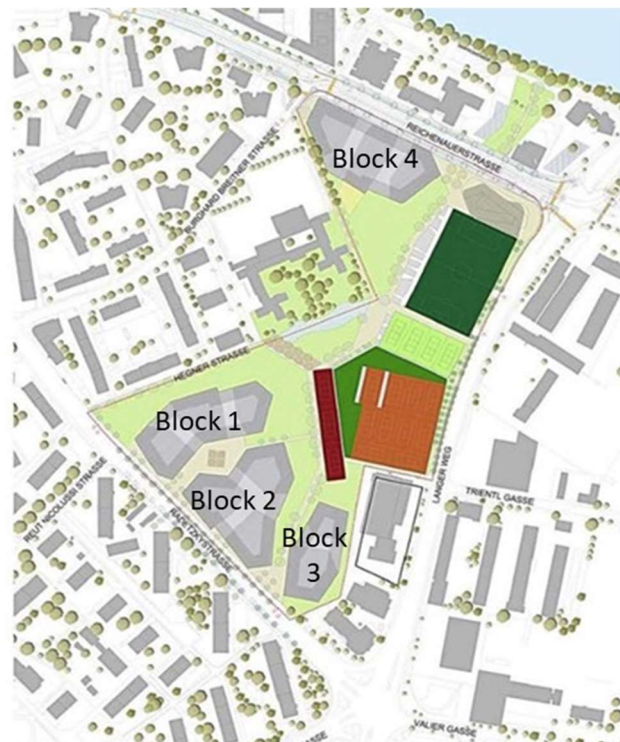


Figure 1: Sketch of the new district Campagne Areal in Innsbruck (ibkinfo.at).

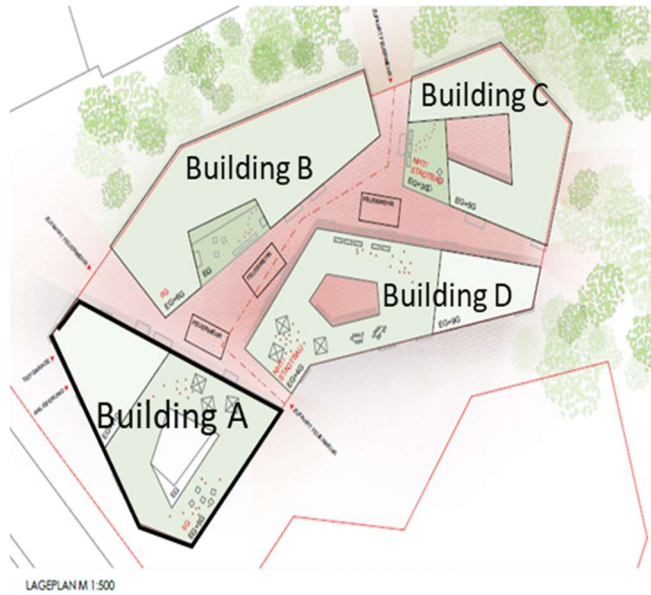


Figure 2: Sketch of the block 1 in Campagne Areal, Innsbruck (ibkinfo.at)

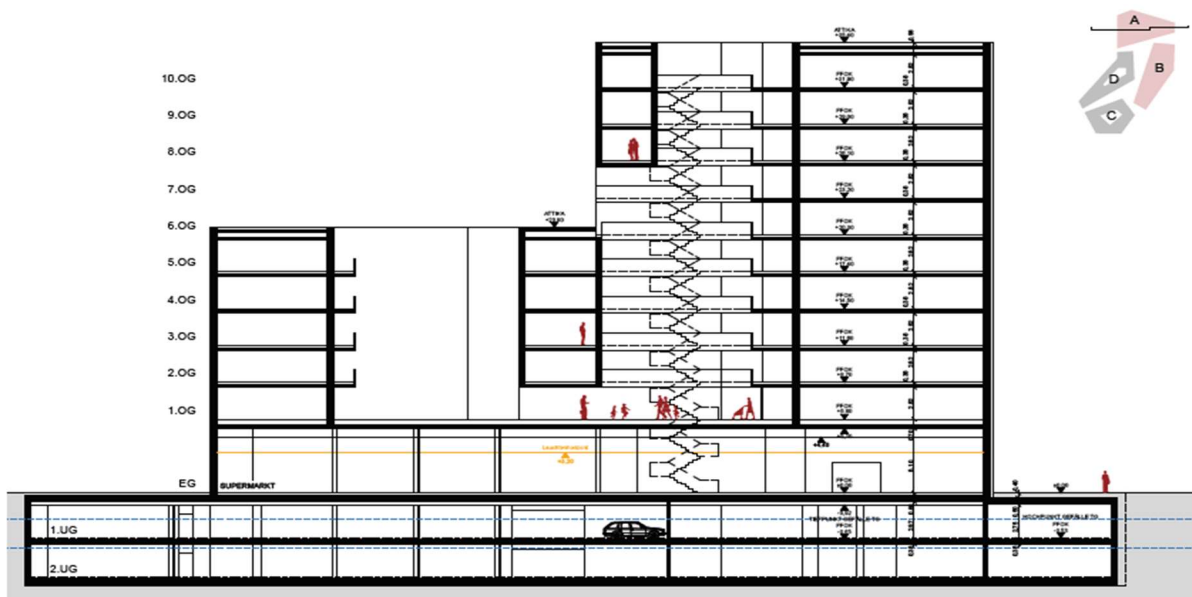


Figure 3: Building A of Block 1

Building A is composed of 96 flats distributed in two portions of the building: one with 11 floors and one with 6 floors.



# Chapter 2. Methodology

## 2.1. Boundaries of the project

Previous studies on the same project show that heat pump heating systems are the best solution in terms of primary energy consumption. However, a Heat Pump system (HP) can hardly supply also DHW (Dermentzis, 2019). Since Austria has grown a lot in the development of District Heating (DH) systems (Sayegh, et al., 2018), it is plausible to consider DH as a source for DHW preparation. The DH system in Innsbruck provides hot water at 90°C. The return flow temperature is 60°C (90/60 DH).

A 4-pipe distribution system has been studied to cover the heating demand and the DHW preparation: 2 pipes are used for the space heating with HP, while 2 pipes are used for the DHW. A scheme of the system is shown in Figure 4.

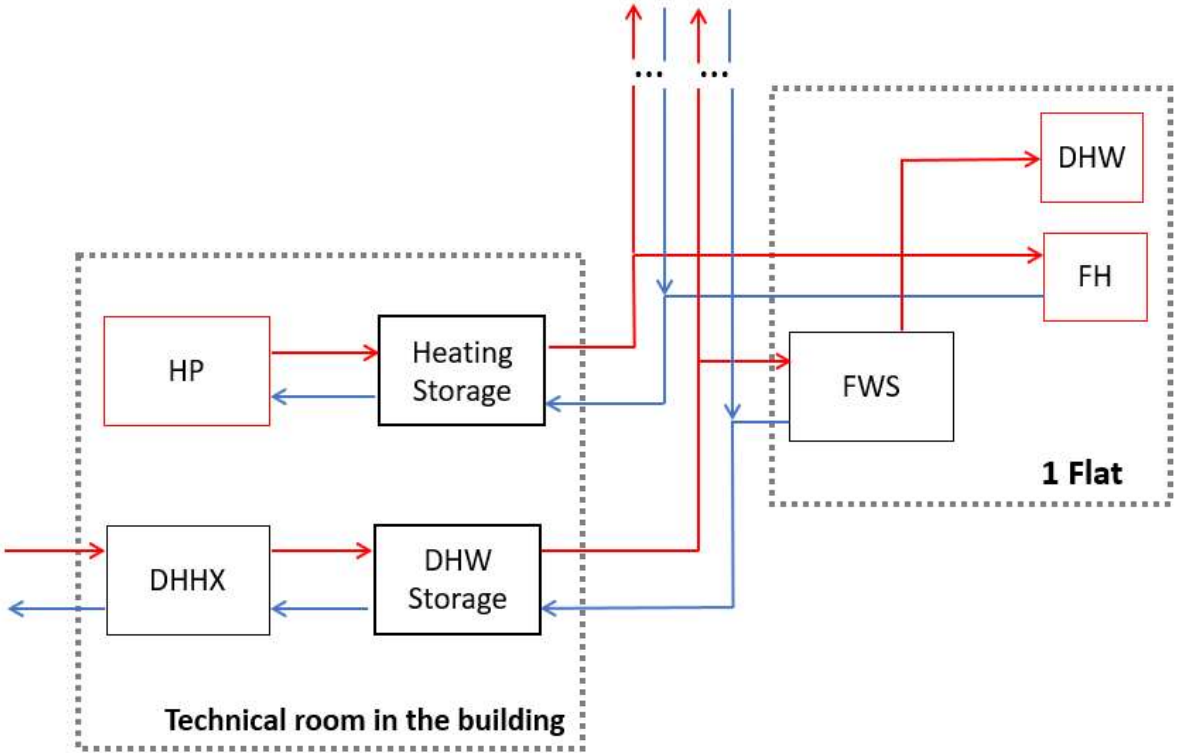


Figure 4: 4-pipe system for Building A in Block 1

A Fresh Water Station (FWS) is placed in each flat in order to provide DHW. The hot source for the FWS is taken from a DHW storage in the technical room, heated up by the DH through

a district heating heat exchanger (DHHX). The space heating, provided by a heat pump, has not been investigated in this work, while DHW preparation from DH is subject of the study.

The technical room is placed in the corner on the left-hand side of the building (see Figure 3). A system of pipes connects the technical room with each flat of the building. Building A has 96 flats and an average number of 2 people per flat is assumed for DHW calculation.

## 2.2. Dynamic simulation tool.

The model for the DHW preparation has been developed in Matlab/Simulink environment in order to carry out dynamic simulations. A method to run a dynamic simulation for a big multi-family building, based on the flat-level DHW preparation model, is then developed.

A dynamic simulation is the first step to design energy-efficient buildings since it takes into account short time variables that would be neglected in a stationary simulation. Thus, the aim of a dynamic simulation is to draw out a set of results over time, which can help the decision-making process for the design of heating and DHW preparation systems. Short time variables are not only the one linked to the DHW usage (which can change second by second), but also all those variables linked to the thermal inertia of the components constituting the DHW preparation system. In Matlab/Simulink, every component of the system can be represented with its own thermal capacity.

Blocks representing hydraulic and thermodynamic components of a DHW production model are taken from the CARNOT ("Conventional And Renewable eNergy systems OpTimization") block-set library. All the blocks are connected in order to communicate with each other through transfer functions.

## 2.3. Simulation models

### 2.3.1. DHW preparation model, flat-level

The model developed in Matlab/Simulink has the purpose to simulate a system to produce DHW for a single flat. Each of the 96 flats of the building has its own FWS for DHW preparation. The study of the FWS in one flat is the starting point of this work: the flat-level HX can be rescaled in order to simulate the supply of DHW to 96 flats with a single central HX.

A simplified hydraulic scheme of the model is shown in Figure 5.

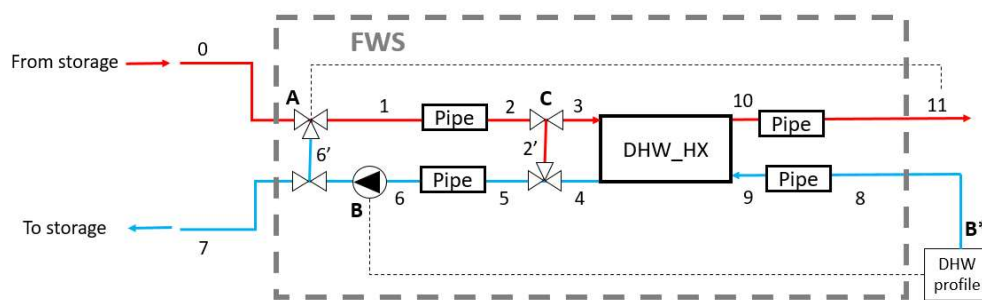


Figure 5: simplified hydraulic scheme of the flat-level system

The hot water entering the FWS comes from a central thermal storage tank placed in the central technical room. In this tank, the energy to supply to all the flats of the building is stored as hot water. The temperature of the water coming from the storage (position 0 in Figure 5) is fixed. The first mixer-diverter (position A) has the purpose to control the required temperature of hot water supplied to the user (position 11) in order to always achieve the set point temperature. The second mixer-diverter (position C) works as a bypass for the HX. The system, in fact, is configured in order to always have a minimum mass flow circulating in the primary side. A bypass of the HX is necessary when there is no mass flow in the secondary side. In this study, the value of the minimum mass flow has a fixed value. However, in reality, this mass flow should be controlled considering that the return temperature to the storage (after the thermal losses in the bypass pipe) should not be too high (around 35°C) in order to avoid high thermal losses in the return pipe to the storage.

Four pipe blocks are placed before and after the FWS in both sides. Pipe blocks are used to simulate thermal behaviour of the pipes and to get stability in the model.

The mass flow circulating in the secondary side is fixed by the DHW user profile (see 2.5). The mass flow circulating in the primary side, instead, is fixed by the circulation pump. The control on the pump is based on a logic linked to the user profile (see 2.4).

FWS includes a cross flow HX. In the primary side, the hot water comes from the storage. In the secondary side the cold water is heated up to the set point temperature.

### 2.3.2. DHW preparation model, building-level

The development of the model for the building-level DHW preparation is based on the flat-level model. A single FWS simulates a central production of DHW for 96 flats. The hydraulic scheme of the model is shown in Figure 6.

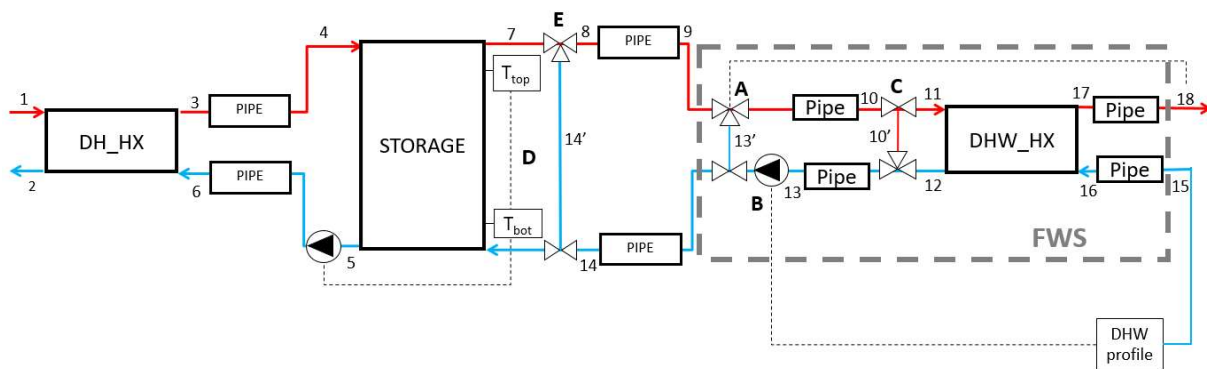


Figure 6: simplified hydraulic scheme of the building-level model

The model can be divided into three branches: storage charging circuit (including positions from 3 to 6 in Figure 6), storage discharging circuit (including positions from 7 to 14), and user circuit (including positions from 15 to 18).

The DH heats up a thermal storage tank. The heat exchange between the water from the DH and the water circulating in the storage charging circuit is realized by a HX (so called district heating heat exchanger DHHX). The DHHX and the storage tank are in the same technical room and the length of the pipes is 3 m. A pump circulates the water in the storage charging circuit.

The storage tank is designed to be heated to 85°C by the hot water produced in the DHHX and it is sized in order to hold all the daily thermal energy required to produce DHW in the building.

Two temperature signals are used to control the circulation pump:  $T_{\text{top}}$  (measured at the top of the tank) and  $T_{\text{bot}}$  (measured at the bottom of the tank).

The storage discharging circuit connects the storage tank to the FWS. In the reality, one FWS is placed in each flat. The sum of the length of the pipes that connect the storage to every single FWS placed in each flat, is equal to 426 m and it is assumed, in the simulation model, as the length of the connection between the storage tank and the central FWS.

Three mixer-diverter couples are used along this path to maintain the designed operative conditions for the HX. The first mixer-diverter (position E in Figure 6) is placed right after the storage tank and it aims to fix the temperature of the hot water out of the storage. The second mixer-diverter, included in the FWS (position A), acts as a controller on the temperature of the DHW supplied to the user (position 18). The third mixer-diverter (position C) is also included in the FWS and it acts as a bypass for the HX.

As already explained for the flat-level model, also for the building model, four pipe blocks are located before and after the HX in both sides to simulate thermal behaviour of the pipes and to get stability in the model.

The mass flow circulating in the user circuit is set according to the user profile. The user profile is also the input for the controller of the circulation pump in the storage discharging circuit (as it is explained in 2.4.4).

## 2.4. Controllers

For the proper development of a model it is essential to well define the controllers. In a typical controller, a set of variables acts as an input for a system that manipulates these variables in order to get an output. The output is called “control signal” and it is used, in these models, as an input for mixers-diverters or pumps. It aims to set the so called “controlled variable” to a set point value.

The FWS model includes two controllers: user mixer-diverter control (position A in Figure 5 and in Figure 6) and storage discharging-pump control (position B in Figure 5 and in Figure 6). These two controllers are included in the FWS and so they are used for both the models: flat-level model and building-level model. A user mass flow control is also used in the flat-level model (position B\* in Figure 5). The building-level model also includes the storage-charging pump control (position D in Figure 6) and storage mixer-diverter control (position E in Figure 6). In the next paragraphs, all these controllers are described.

### 2.4.1. Storage charging-pump controller

This controller is used to set the mass flow in the storage charging circuit. The mass flow is controlled in order to always get the set point temperature in the whole storage tank. Thus, the control signal is an input for the storage charging pump and the controlled variable is the mass flow.

Two values of temperature are the inputs of the controller: the temperature  $T_{top}$  of the water at the top of the storage tank, and the temperature  $T_{bot}$  of the water at the bottom of the tank. The scheme of the controller is shown in Figure 7.

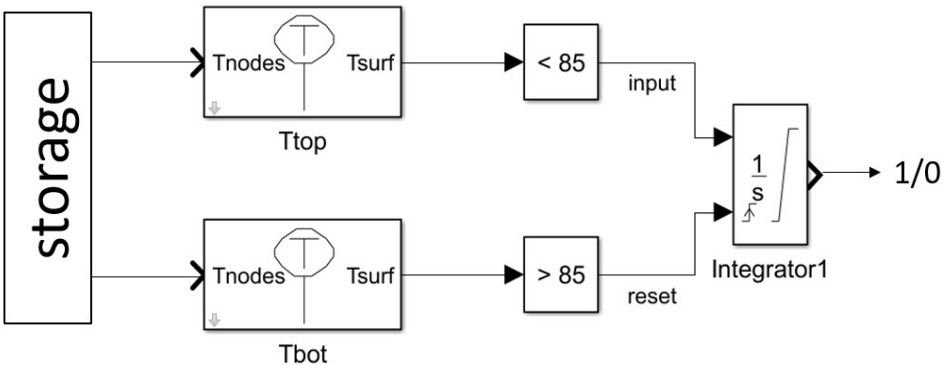


Figure 7: scheme of the storage charging pump controller

These two values of temperature are then compared to the set point, giving a boolean output (1 or 0 if the comparison is, respectively, true or false). The boolean outputs from the comparison are the “input” and “reset” values of an integrator. The “input” signal is the value that is integrated. With regard to the “reset” value, every time the  $T_{top}$  switches from  $T_{top} < 85^{\circ}\text{C}$  to  $T_{top} \geq 85^{\circ}\text{C}$ , it switches from 0 to 1 and it resets the initial value of the integral to 0.

Two cases are presented in Table 1. In both cases  $T_{bot}$  is switching from a  $T < 85^{\circ}\text{C}$  to  $T = 85^{\circ}\text{C}$ , resetting the initial value to 0.

In Case 1  $T_{top} > 85^{\circ}\text{C}$ . The “reset” signal fixes the initial condition of the integral back to 0: the output of the integral is 0 and stops the pump.

In Case 2  $T_{top} < 85^{\circ}\text{C}$ . The “reset” signal fixes the initial condition of the integral back to 0: the output of the integral is 1 and it activates the pump.

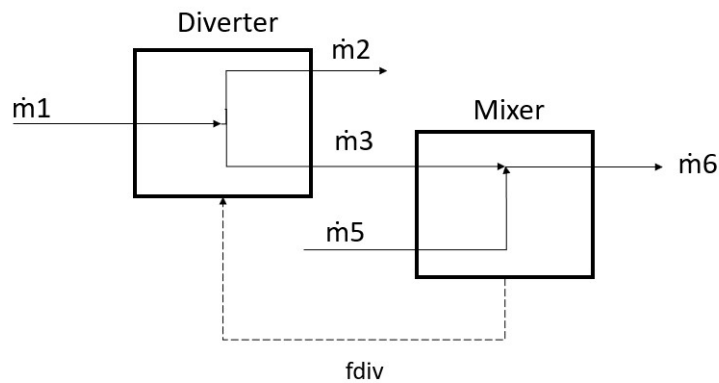
These two cases are summarised in Table 1.

*Table 1: reaction of the control in two simple cases*

|        | $T_{top} < 85^{\circ}\text{C}$ | Reset to initial condition | Output |
|--------|--------------------------------|----------------------------|--------|
| Case 1 | 0                              | Reset to 0                 | 0      |
| Case 2 | 1                              | Reset to 0                 | 1      |

## 2.4.2. Mixer-diverter controller

This is a temperature controller and it is used to limit the temperature of the water in certain branches of the circuit. The controller is composed by a mixer and diverter as it is shown in Figure 8.



*Figure 8: simplified scheme of mixer–diverter controller*

The controlled variable is the temperature of the fluid that comes out from the mixer. The control signal is called  $fdiv$  and it is elaborated by the mixer, based on the difference between the temperature to control and a set point temperature as it is possible to see from the scheme in Figure 9.

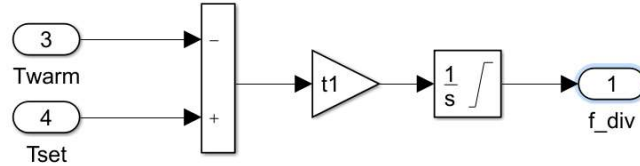


Figure 9:  $f\_div$  calculation block from CARNOT

The error is also multiplied by a constant called  $t1$  and then integrated in order to create the  $fdiv$  signal. The smaller the constant  $t1$ , the sooner the system reaches the stability after the action of the control.  $fdiv$  is in the range between 0 and 1 and it acts on the diverter, setting the percentage of the fluid that is diverted to the mixer. The mass flows are set according to the following equations referred to the scheme in Figure 8

$$\dot{m}_2 = \dot{m}_1 \cdot fdiv \quad (1)$$

$$\dot{m}_3 = \dot{m}_1 \cdot (1 - fdiv) \quad (2)$$

One mixer-diverter controller (called storage mixer-diverter controller) is included in the building-level model and it is placed right after the storage in the storage discharging circuit (position D in Figure 6). The controlled temperature is the one of the water sent to the FWS.

A mixer-diverter controller (called user mixer-diverter control) is also included in the FWS and so it is used in both the models (position A in Figure 5 and Figure 6). The controlled variable is the DHW supply temperature (position 11 in Figure 5 and position 18 in Figure 6). In this case, this temperature is controlled indirectly. The controller, in facts, does not changes directly the temperature of DHW supply, but it changes the temperature of the water entering the HX in the primary side (position 3 in Figure 5 and position 11 in Figure 6) in order to get the set point temperature in the DHW supply.



### 2.4.3. Storage discharging-pump controller

This controller is used to set the mass flow in the storage discharging circuit. The value of this mass flow is set in order to provide, to the HX, the hot source to achieve the requests.

Thus, the control signal is an input for the storage discharging pump and the controlled variable is the mass flow. The control signal, in the range between 0 and 1, acts on the pump fixing the percentage of the design value of the mass flow circulating. Two different discharging-pump strategies are considered: on-off control and proportional control:

- 1) The on-off control takes as input the value of the mass flow defined by the user profile and fixes the control signal to 1 (if the user is asking for DHW) or to “minimum” (if the user is not asking for DHW). 1 means that 100% of the designed mass flow circulates in the storage-discharging circuit, while “minimum” means that the mass flow circulating is at a fixed minimum value.
- 2) The proportional control takes as input the value of the mass flow defined by the user profile. The controller elaborates an input signal on the pump that is between 1 and a minimum value. The signal 1 is obtained during the peak request and it fixes the mass flow on the storage-discharging circuit to the design value. When there is no DHW request by the user, the controller elaborates a minimum value for the input signal of the pump, in order to set the mass flow circulating in the circuit to a minimum value, ensuring the minimum mass flow circulating in the primary side of the FWS.

### 2.4.4. User mass flow controller

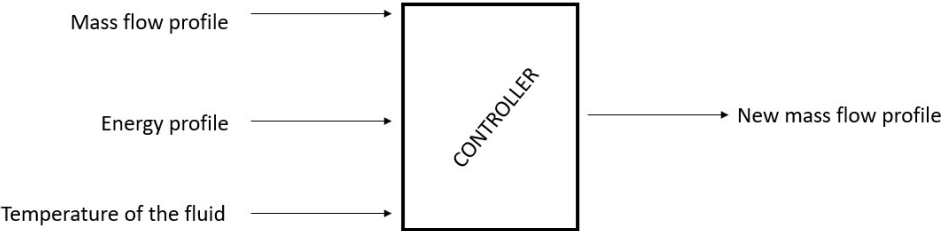
This control is only used in the flat-level model and it aims to achieve the thermal energy request by the user (achievement of useful energy). The controller sets the duration of the tappings creating a user mass flow profile. The duration of each tapping is calculated with the following equation:

$$duration = \frac{Q}{\dot{m} \cdot c_p \cdot \Delta\theta} \quad (3)$$

Where  $Q$  [kWh/tapping] is the energy supplied to the user by each tapping;  $\dot{m}$  [kg/(s·tapping)] is the mass flow of each tapping based on the DHW profile;  $\Delta\theta$  is the temperature difference

between the cold water and the set point of the supplied DHW. In the first seconds of tappings, the mass flow supplied is at a temperature lower than the set point. The energy supplied in these seconds is not counted as useful energy. It means that the duration of each tapping can be longer lasting than the duration required by the original profile. Based on the calculated duration of the tappings, a new mass flow profile is created.

A simplified scheme, considering the input and the output of the controller, is shown in Figure 10.



*Figure 10: input and output of the user mass flow controller*

## 2.5. DHW profiles

The DHW profile strictly depends on the behaviour of the occupants of the house. For flat-level model and for building-level model, different profiles are described, aiming to check the influence of the profile on the simulation results. The profiles are either based on the standard EN16147, profile M (where a daily tapping cycle is described), or created as stochastic profiles with DHWcalc tool.

### 2.5.1. Standard EN16147

The standard EN16147 lists the tappings occurring during one day in a typical 4-people apartment. The profile M for the standard is considered. For each tapping, the starting time, the energy required and the volume flow are given.

The tapping cycle derived from the standard EN16147 includes three kinds of tappings: small tapping, shower (occurring twice per day) and dish washing. The mass flow [kg/s] from each tapping is derived by the volume flow listed in the standard EN16147 in l/min. The set point of the DHW supplied to the user is considered to be at 45°C while the cold water is considered to be at 10°C:  $\Delta\theta = 35$  °C. From  $\Delta\theta$  and from the mass flow, it is possible to calculate the power associated to each tapping ( $\dot{Q}$ ) with Equation 14. Once the power of each tapping is calculated, it is divided by the energy given by the standard EN16147 in order to obtain the information about the duration of each tapping.

All the information taken or calculated from the standard EN16147 are summarized in *Table 2*:

Table 2: daily tapping cycle based on the standard EN16147

| Time of day | E [kWh] | $\dot{V}$ [l/min] | $\dot{m}$ [kg/s] | $\dot{Q}$ [kW] | Duration [s] |
|-------------|---------|-------------------|------------------|----------------|--------------|
| 07:00       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 07:15       | 1.4     | 10                | <b>0.17</b>      | <b>24.32</b>   | <b>207</b>   |
| 07:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 08:00       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 08:15       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 08:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 08:45       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 09:00       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 09:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 10:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 11:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 11:45       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 12:45       | 0.315   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>117</b>   |
| 14:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 15:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 16:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 18:00       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 18:15       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 18:30       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 19:00       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 20:30       | 0.735   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>272</b>   |
| 21:15       | 0.105   | 4                 | <b>0.07</b>      | <b>9.73</b>    | <b>39</b>    |
| 21:30       | 1.4     | 10                | <b>0.17</b>      | <b>24.32</b>   | <b>207</b>   |

In the period between 21:30 and 7:00 no tapplings occur. The value of the daily thermal energy request obtained from the standard EN16147 is the sum of the energy taken from each tapping and it is equal to 5.8 kWh/day (useful energy).

## 2.5.2. Stochastic profile

A stochastic profile can be generated using DHWcalc tool. The profile is based on statistics, distributing DHW tapplings throughout a fixed period, following a probability function. The user can set the reference conditions such as volume of DHW required daily, duration of the tapplings, daily probabilities. Total mean daily draw-off volume in l/day is fixed according to the information derived from the standard EN16147. For a long period-simulation, probability seasonal variations, weekend variations and holiday periods can be set. The tool can be used to create either a profile per each flat separately or a profile for the whole building. The profiles are given as text files containing all the information related to the tapplings.

## 2.5.3. Simultaneity factor

In order to evaluate a building profile for the building-level DHW preparation model, one approach would be to consider the same DHW profile for all the flats. In this case the tapplings for each flat would be considered occurring at the same time and the peak load for the building would be the sum of the peak load of each flat. However, in reality, the loads for every single flat do not occur at the same time. This is the reason why this approach cannot be considered. A simultaneity factor  $f_s$  is taken into account in these simulations. The simultaneity factor is calculated as follow:

$$f_s = \frac{\text{Building peak load}}{\sum_i \text{flat peak load}_i} \quad (4)$$

The denominator of the ratio is the sum of the maximum load daily asked by each flat. The numerator is the daily peak load of the building. As already mentioned, the peak loads for each flat do not occur at the same time, this is the reason why the building peak load differs from the sum of the flat peak loads. This difference changes according on how the building-level profile is implemented from the flat-level profile.

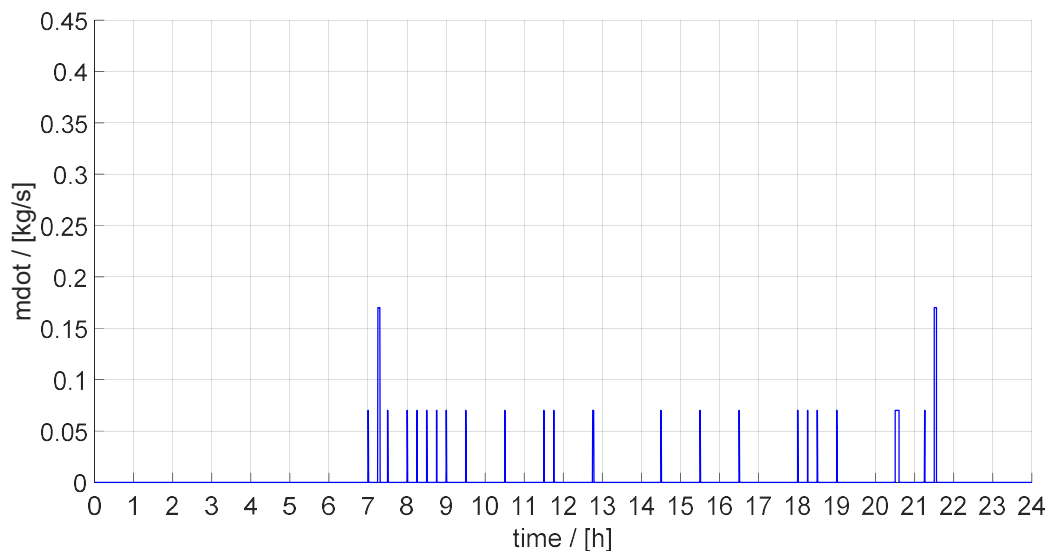
If the flat peak loads occur simultaneously, their sum is equal to the building peak load and  $f_s$  is equal to 1, otherwise  $f_s$  is lower than 1.

## 2.5.4. Implemented DHW profiles

### 2.5.4.1. Flat-level

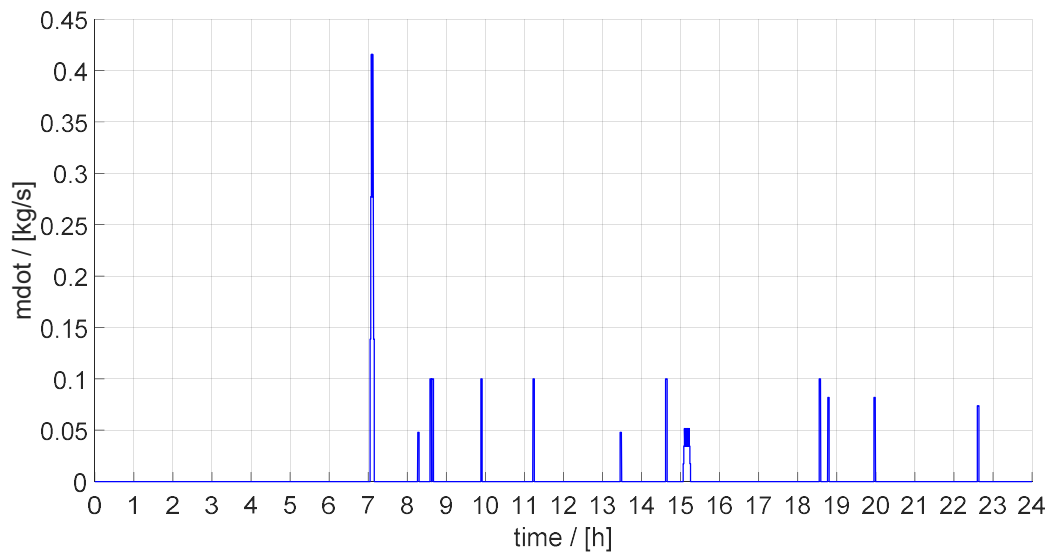
For the flat-level model, two DHW profiles are tested:

- 1) One profile derives from the standard EN16147 (profile M). With this DHW profile, 5.8 kWh/day is the daily useful energy requested by the user. Two peaks (0.17 kg/s) occur at 7:15 and 21:30 and they are due to the showers. The duration of the tappings has been already shown in *Table 2*. No tappings occur during the night between 21:30 and 7:00. The trend of this profile is shown in Figure 11.



*Figure 11: DHW profile from standard EN 16147, single flat-level*

- 2) Stochastic profile derives from DHWcalc, considering 144 l/day as daily DHW draw-off volume, in order to supply 5.8 kWh/day of useful energy to the user. The profile is generated for one day and the tapplings are randomly distributed all over the day. The mass flow of the first tapping occurring in the morning is equal to 0.42 kg/s. No tapplings occur during the night between 22:30 and 7:00. The trend of this profile is shown in Figure 12.



*Figure 12: stochastic DHW profile, single flat-level*

#### 2.5.4.2. Building-level

In order to simulate the influence of the DHW profiles on the results, four different building profiles are tested: two of them are derived from the standard EN16147, two are created with DHWcalc.

An average number of two people per flat is considered for the creation of the building profiles. The four building DHW profiles are here listed:

- 1) Hourly average profile. From standard EN16147, profile M, the energy requested of the building from each tapping is spread over one hour. The peak load for the DHW (occurring from 7:00 to 8:00 and from 21:00 to 22:00) is calculated assuming a simultaneity factor equal to 0.2 and the reduced energy in the peak power is added in the hour before the first peak (from 6:00 to 7:00) and after the last peak (from 22:00 to 23:00) (Dermentzis, 2019). The sum of the individual mass flow peaks is equal to 16.32 kg/s, while the value of the maximum mass flow with this profile is equal to 0.36 kg/s, then the simultaneity factor is 0.02. The resulting profile is shown in Figure 13.

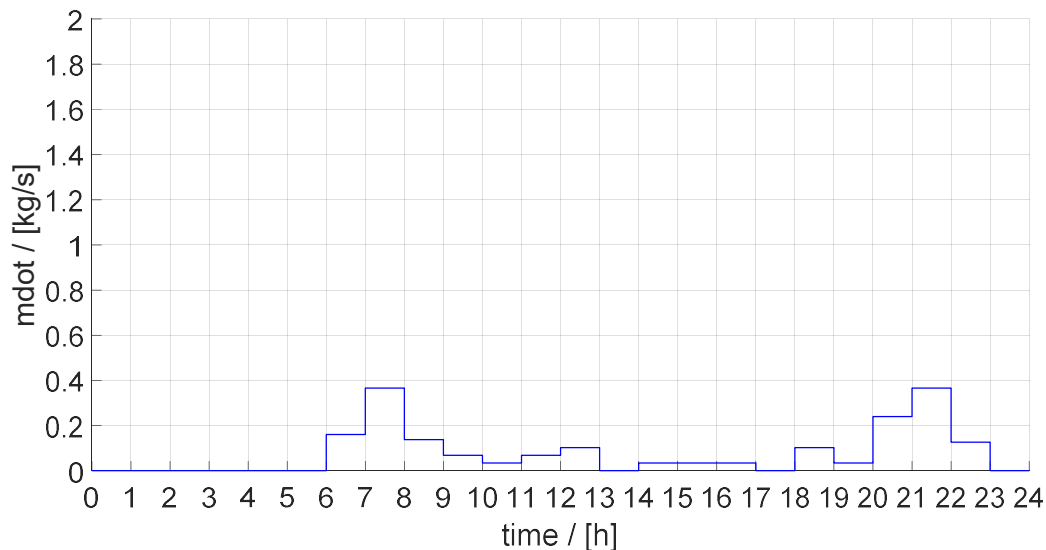
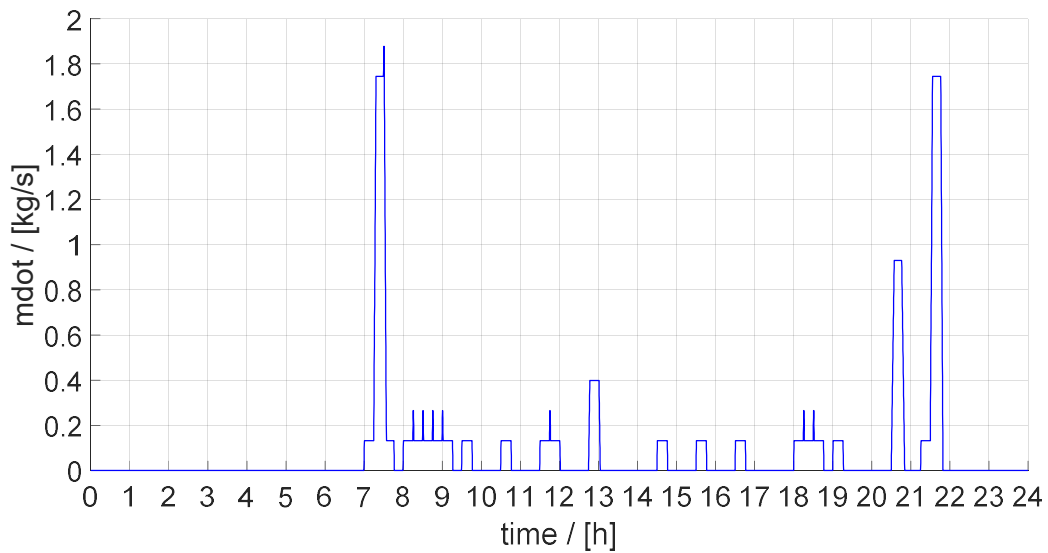


Figure 13: hourly average profile, building-level



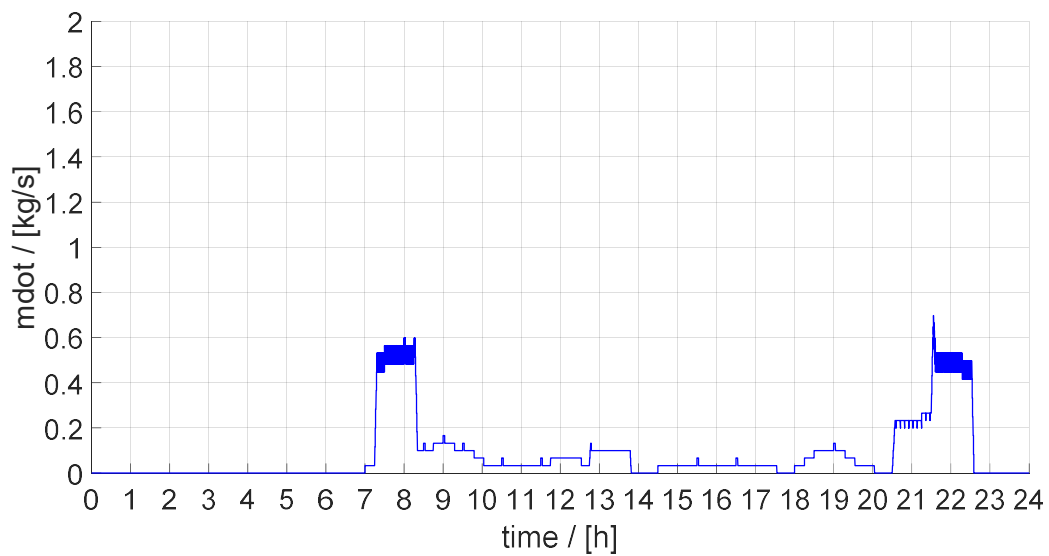
2) 10 seconds profile. The reference is the standard EN16147, profile M. A single flat profile is derived from the standard. In the implementation of the profile in the building model, a delay of 10 seconds on the starting time of the daily tapping routine of each flat is considered. It means that, if the first tapping for the first flat occurs at 7:00:00, the first tapping for the second flat occurs 10 s after, at 7:00:10. The first tapping for the 96<sup>th</sup> flat occurs after 960 s from the first one, at 7:16:00. The value of the maximum mass flow with this profile is equal to 1.91 kg/s. The simultaneity factor in this case is equal to 0.12.

This profile is shown in Figure 14.



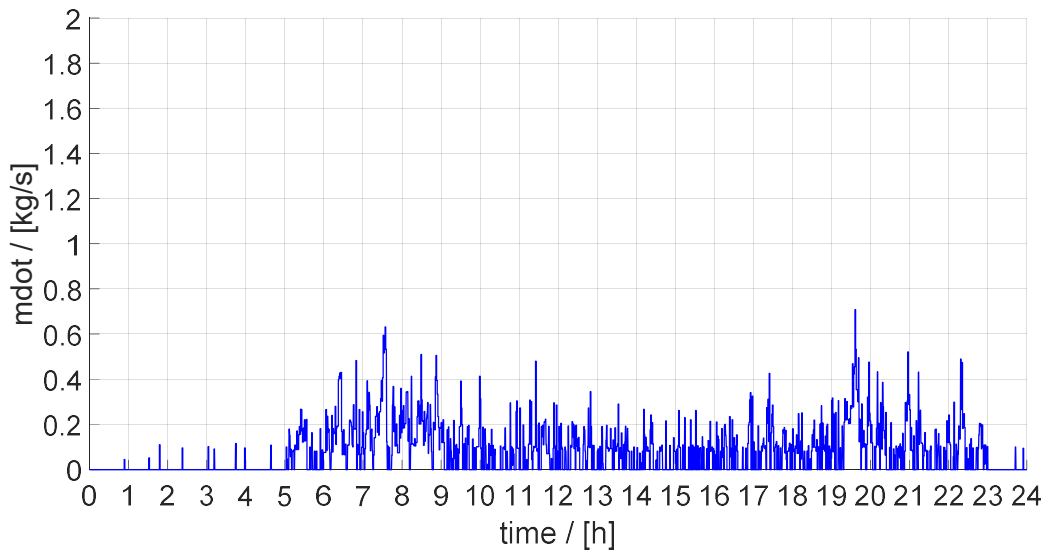
*Figure 14: 10 seconds profile, building-level*

- 3) 39 seconds profile. Also in this case, a profile for a single flat is derived from the standard EN16147, profile M. The delay on the starting time of the daily tapping routine for each flat is 39 s, which is the duration of a small tapping (see *Table 2*). The starting time for the daily tapping routine of the first flat is 7:00:00, while the starting time for the 96<sup>th</sup> flat is 8:02:24. The value of the maximum mass flow with this profile is equal to 0.69 kg/s and the simultaneity factor is equal to 0.04. The profile is shown in Figure 15.



*Figure 15: 39 seconds profile, building-level*

- 4) Stochastic profile. DHWcalc tool is used to generate a stochastic building profile. The profile is generated for one day and it spreads the daily tappings all over the day. The total draw-off volume per day is derived from the standard EN16147, multiplying the daily DHW volume used in a 2-people flat, for the number of flats of the building. The value of the maximum mass flow with this profile is equal to 0.70 kg/s. Also considering the sum of the individual mass flow peaks equal to 16.32 kg/s the simultaneity factor for this profile is equal to 0.04. The profile is shown in Figure 16.



*Figure 16: stochastic DHW profile, building-level*

Table 3 summarises the simultaneity factor for the four different building profiles.

*Table 3: simultaneity factor with the four different building profiles*

|    | Hourly average profile | 10s profile | 39s profile | Stochastic profile |
|----|------------------------|-------------|-------------|--------------------|
| fs | 0.02                   | 0.12        | 0.04        | 0.04               |

## 2.6. Parametrization of the models

### 2.6.1. Flat-level model

A flat with 4 occupants, with a useful energy request equal to 5.8 kWh/day, is considered for the simulations. The temperature of the water coming from the storage is fixed at 52°C (position 0 in Figure 5). No storage is simulated in the flat-level model. The water in the secondary side of the HX is taken as cold water at 10°C (position 8 in Figure 5) and it is heated up to 45°C (position 11). The temperature of the water out of the HX in the primary side (position 4) is the only temperature that is not fixed.

A temperature not higher than 30°C is desirable for the water out of the HX in the primary side (position 4). This water, after the exchange, still holds thermal energy and it causes non-neglectable thermal losses in the return pipe to the storage tank.

The four 1-m pipes located in each branch of both sides of the FWS have a small capacity (100 J/(m·K)) and high thermal losses (5 W/(m·K)) so that, when there is no DHW request from the user, the water contained in these pipes reaches the room temperature (fixed at 20°C).

A 35-kW HX is chosen, based on common practise. Based on the characteristics derived from the data sheet of Danfoss, three parameters of the HX are calculated: the heat transfer coefficient between the two sides of the HX  $UA_{HX}$  [W/K], the thermal capacity  $C$  [J/K] and the heat losses coefficient  $UA_{HL}$  [W/K].

$UA_{HX}$  value is calculated with the following equation.

$$UA_{HX} = \frac{\dot{Q}}{\Delta\theta_{log}} \left[ \frac{W}{K} \right] \quad (5)$$

Where  $\dot{Q}$  is the power of the chosen HX, while  $\Delta\theta_{log}$  is calculated as follow:

$$\Delta\theta_{log} = \frac{(\Delta\theta_1 - \Delta\theta_2)}{\ln(\Delta\theta_1/\Delta\theta_2)} \quad (6)$$

Where:

$$\Delta\theta_1 = \theta_{primary\_out} - \theta_{secondary\_in} \quad (7)$$

$$\Delta\theta_2 = \theta_{primary\_in} - \theta_{secondary\_out} \quad (8)$$

*primary\_in* and *primary\_out* are referred respectively to the inlet and outlet of the primary side HX, while *secondary\_in* and *secondary\_out* are referred to the inlet and outlet of the secondary side of the HX.

The thermal capacity  $C$  [J/K] is calculated with the following equation.

$$C = cp \cdot m \quad (9)$$

Where  $cp$  is the thermal capacity of the stainless steel ( $cp_{\text{stainless\_steel}} = 502$  J/kgK) and  $m$  is the mass of the HX shown in Table 4.

Heat transfer coefficient with the ambient  $UA_{HL}$  [W/K] is calculated from the thickness of the insulant  $s$ , its thermal conductivity  $\lambda$  and the total external surface  $S$  of the HX (listed in Table 4) with the following Equation 9.

$$UA_{HL} = \frac{\lambda}{s} \cdot S \quad (10)$$

Figure 17 shows a simplified representation of the HX.

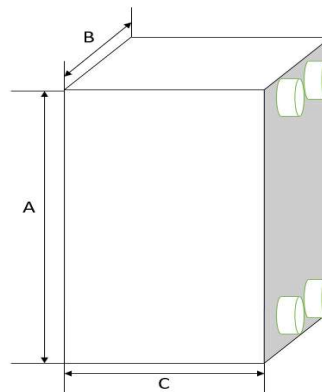


Figure 17: simple representation of the HX

Table 4 summarizes the main characteristics of the HX chosen by the catalogue of Danfoss

Table 4: characteristics of the HX

|             |       |
|-------------|-------|
| Model of HX | XB51L |
| A [m]       | 0.466 |
| B [m]       | 0.256 |
| C [m]       | 0.064 |

|   |                 |
|---|-----------------|
| External surface S [m <sup>2</sup> ]        | 0.331           |
| m [kg]                                      | 15.60           |
| Number of plates                            | 20              |
| Material of plates                          | Stainless steel |
| Total exchange surface [m <sup>2</sup> ]    | 1.89            |
| Thickness insulation s [m]                  | 0.02            |
| Thermal conductivity of insulation λ [W/mK] | 0.04            |
| <b>UA<sub>HX</sub> [W/K]</b>                | <b>1050</b>     |
| <b>C<sub>HX</sub> [J/K]</b>                 | <b>7831</b>     |
| <b>UA<sub>HL</sub> [W/K]</b>                | <b>0.58</b>     |

As already mentioned, two different user profiles are considered: the one given by the standard EN 16147 and the stochastic profile. Also, two different control for the circulation pump are tested: on-off and proportional control. Four different cases can be simulated, as shown in Table 5.

*Table 5: single flat analysed cases*

|        | Profile    | Pump control |
|--------|------------|--------------|
| Case 1 | EN 16147   | On-Off       |
| Case 2 | EN 16147   | Proportional |
| Case 3 | Stochastic | On-Off       |
| Case 4 | Stochastic | Proportional |

In this model, no distribution system from/to the storage is considered, thus no considerations about thermal losses in the pipes can be made.

The model of the HX chosen from CARNOT library calculates the outlet temperatures referring on the inlet temperatures using the following equations taken from the CARNOT user guide:

$$\theta_{hot\_out} = \theta_{hot\_in} - \Psi \cdot (\theta_{hot\_in} - \theta_{cold\_in}) \quad (11)$$

$$\theta_{cold\_out} = \theta_{cold\_in} - \frac{W_{hot}}{W_{cold}} \cdot (\theta_{hot\_in} - \theta_{hot\_out}) \quad (12)$$

Where  $\Psi$  is a parameter called “dimensionless temperature change”, while  $W_{\text{hot}}$  and  $W_{\text{cold}}$  are the product between the mass flow and the capacity of the fluid in the two sides of the HX expressed in W/K.

## 2.6.2. Building-level model

The daily thermal energy required by the building is equal to 280 kWh/day. This is the base data used to size the storage thermal tank which is simulated in the building model. The volume  $V$  [m<sup>3</sup>] of the storage tank, necessary to store the daily thermal energy, is calculated with the following equation.

$$V = \frac{Q}{\rho \cdot cp \cdot \Delta\theta} \quad (13)$$

Where:

$Q = 280$  kWh/day is the daily thermal energy stored in the tank;

$\rho$  = is the value of water density;

$cp$  = is water specific heat capacity;

$\Delta\theta$  = is the temperature difference between the hot water filling the tank (position 4 in Figure 6) and the cold water leaving the tank (position 5 in Figure 6).

In respect to Equation 13, fixing  $\Delta\theta = 60$  K, a 4 m<sup>3</sup> thermal storage tank is chosen. The diameter of the tank is supposed to be 2 m. The heat losses of the walls of the storage tank are taken from the PHPP and they are equal to 5.5 W/K. Geometrical and thermal characteristics of the tank are summarized in the Table 6.

*Table 6: Geometrical and thermal characteristics of the storage tank*

|                     | Surface [m <sup>2</sup> ] | Heat losses coefficient [W/m <sup>2</sup> K] |
|---------------------|---------------------------|--|
| Top cover           | 3.14                      | 1.2  |
| Bottom              | 3.14                      | 1.2  |
| Cylindrical surface | 8                         | 3.08   |

The set point temperature of the storage is constantly 85°C.

All the distribution pipes of the building are considered in a single pipe connecting the storage tank to the central HX. As already mentioned in 2.3.2, this pipe is considered to be 426 m

(Dermentzis, 2019). The diameter of the pipes is considered to be 3.5 cm. The insulation of the pipe is considered with a heat transfer to the ambient coefficient equal to 0.227 W/(m·K) (Dermentzis, 2019). The thermal capacity of the pipes is 1440 J/(m·K) as a typical value of thermal capacity of the pipes taken from data sheets. Four 1-m pipes (with high losses equal to 5 W/(m·K) and low thermal capacity of 100 J/(m·K)) are placed in each branch of the FWS in order to give stability to the systems and to let the fluid reach the temperature of the room while no mass flow is circulating.

For the storage-discharging pump control, only the proportional control is tested.

Once the user mass flow profile is predicted, the maximum load of the HX is fixed. From the peak of the DHW mass flow supplied to the user (and so the peak load), it is possible to calculate the power  $\dot{Q}$  [W] of the HX with the following equation.

$$\dot{Q} = \dot{m} \cdot c_p \cdot \Delta\theta \quad (14)$$

Where:

- $\dot{m}$  [kg/s] is the maximum DHW mass flow supplied to the user;
- $c_p$  is the water thermal capacity;
- $\Delta\theta$  is the temperature difference between the cold water and the DHW supplied to the user.

The parametrization of the HX for the building is based on the peak loads: it gives different values depending on the chosen DHW profile and so on the simultaneity factor. Figure 18 shows the different building peak load obtained considering or not considering the simultaneity factor.

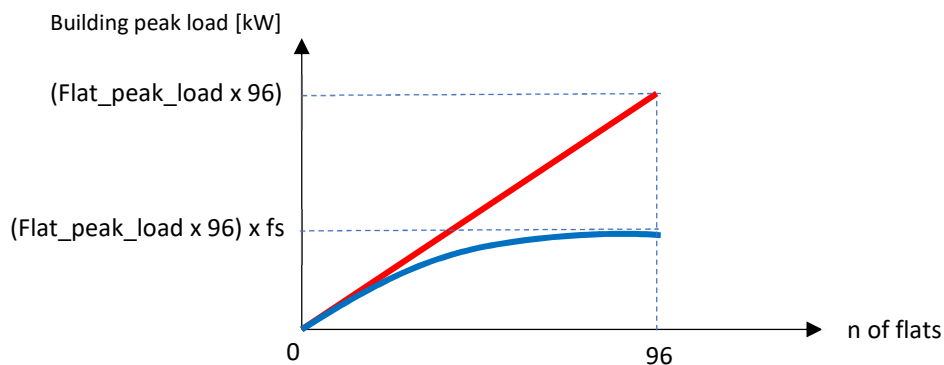


Figure 18: difference between the peak load calculated considering or not considering the fs



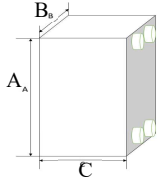
Table 7 summarizes the 4 different user DHW profiles considered in this work for the building-level model, with the simultaneity factor associated to each profile and the calculated values of  $\dot{Q}$  (Equation 13) and  $UA_{HX}$  (Equation 4) of the HX.

Table 7: list of user profiles with  $f_s$  and calculate values of  $\dot{Q}$  and  $UA_{HX}$  for each profile.

| Name of the profile            | Maximum $\dot{m}$ [kg/s] | $f_s$ | $\dot{Q}$<br>[kW] | $UA_{HX}$<br>[W/K] |
|--------------------------------|--------------------------|-------|-------------------|--------------------|
| Case 1: Hourly average profile | 0.37                     | 0.02  | <b>53</b>         | <b>4280</b>        |
| Case 2: 10 seconds profile     | 1.91                     | 0.12  | <b>280</b>        | <b>22612</b>       |
| Case 3: 39 seconds profile     | 0.69                     | 0.04  | <b>101</b>        | <b>8156</b>        |
| Case 4: Stochastic profile     | 0.71                     | 0.04  | <b>104</b>        | <b>8399</b>        |

Based on Table 7 it is possible to parametrize the HX in four cases which differ with respect to the user DHW profile. In each case, a different value of thermal capacity of the HX is calculated, in order to approximate a realistic behaviour of 96 HXs together. The parametrization of the HX in each case is summarised in Table 8.

Table 8: characteristics of the HX in each case

| Characteristics   | Case 1          | Case 2          | Case 3          | Case 4          |
|---|-----------------|-----------------|-----------------|-----------------|
| Model of HX   | XB51L           | XB51L           | XB51L           | XB51L           |
|  A [m] | 0.466           | 0.466           | 0.466           | 0.466           |
| B [m]   | 0.256           | 0.256           | 0.256           | 0.256           |
| C [m]   | 0.106           | 0.220           | 0.142           | 0.142           |
| External surface S [m <sup>2</sup> ]  | 0.392           | 0.556           | 0.444           | 0.444           |
| m [kg]  | 21.68           | 38.40           | 27              | 27              |
| Number of plates  | 36              | 80              | 50              | 50              |
| Material of plates  | Stainless steel | Stainless steel | Stainless steel | Stainless steel |
| Total exchange surface S [m <sup>2</sup> ]  | 3.57            | 8.19            | 5.04            | 5.04            |
| Thickness insulation s [m]  | 0.02            | 0.02            | 0.02            | 0.02            |
| Thermal conductivity of insulation<br>$\lambda$ [W/mK]                                    | 0.04            | 0.04            | 0.04            | 0.04            |
| $C_{HX}$ [J/K]  | <b>10883</b>    | <b>19277</b>    | <b>13554</b>    | <b>13554</b>    |
| $UA_{HL}$ [W/K]   | <b>0.69</b>     | <b>0.97</b>     | <b>0.78</b>     | <b>0.78</b>     |

# Chapter 3. Results

The following key performance indicators are considered:

- *Useful energy* UE, i.e. the amount of energy supplied to the user;
- *Final energy* FE, i.e. the energy taken from the DH;
- *Losses*, as the difference between FE and UE;
- $\theta_{DHW}$ , i.e. the temperature of the water supplied to the user;
- $\theta_{return}$ , i.e. the temperature of the water sent back to the storage from the FWS;
- *Waiting time*, i.e. the time that the DHW needs to reach the set point temperature, as it is shown in Figure 19.

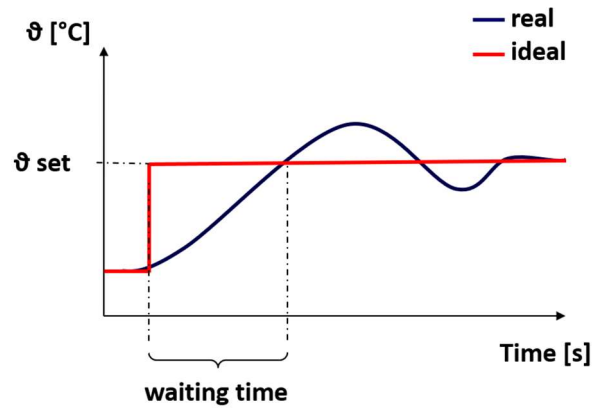


Figure 19: waiting time to reach the DHW  $\theta$  set point

For the flat-level DHW production model, the logic of the control of the pump and the DHW profiles are the variables for the simulations. The simulations aim to get information about the achievement of the required useful energy and about the comfort which includes analysis of the temperature development and the dynamic behaviour as it is shown in the scheme in Figure 20.

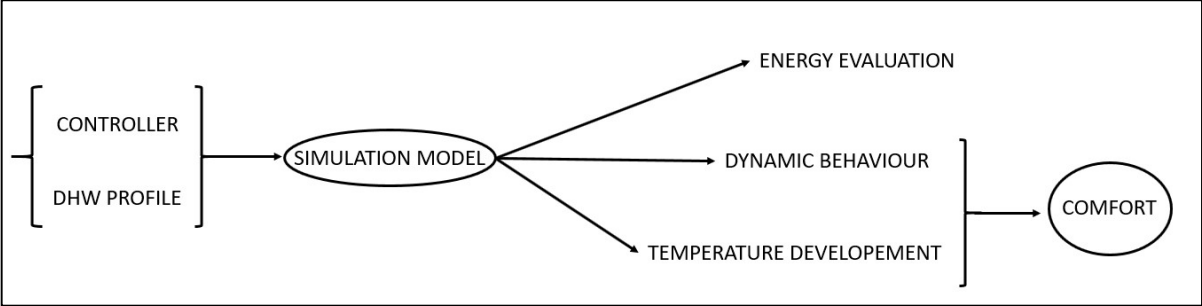


Figure 20: scheme of the methodology used in the flat-level simulations

For the building-level DHW preparation model, DHW profiles and the size of the HX are the variables for the simulations. The results regarding the achievement of the required useful energy, the temperature development and the dynamic behaviour allow to evaluate the comfort. The return temperature to the storage is analysed. With the building-level DHW preparation model, the temperature development also allows to get information about the pipe losses, as it is shown in Figure 21.

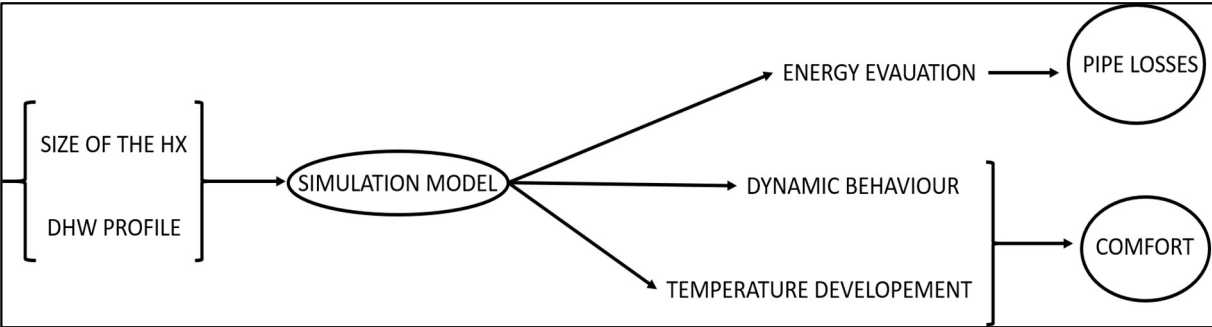


Figure 21: scheme of the methodology used in the building-level simulations

## 3.1. Results of the flat-level model

Table 9 summarises the simulation cases for the flat-level DHW preparation.

*Table 9: simulation cases for flat-level DHW preparation*

| FLAT-LEVEL |   |
|------------|---|
| Case 1     | Standard EN16147 profile + on-off control       |
| Case 2     | Standard EN16147 profile + proportional control |
| Case 3     | Stochastic profile + on-off control             |
| Case 4     | Stochastic profile + proportional control       |

According to Table 9 the DHW profile and the logic of the control of the pump varies in the 4 cases, while the parametrization of the HX does not change in the 4 cases.

Referring to Figure 5 the following temperatures are analysed:

- water from storage, “*From\_storage*”, position 0;
- water entering in the primary side of the HX, “*Pri\_in*”, position 3;
- water going out from the primary side of the HX, “*Pri\_out*”, position 4;
- water entering in the secondary side of the HX, “*Sec\_in*”, position 9;
- DHW temperature, “*Sec\_out*”, position 11;
- water to storage, “*To\_storage*”, position 7.

The trend of the mass flow circulating in the FWS is also analysed, referring to Figure 5:

- mass flow circulating in the primary side of the HX, “*primary*”;
- mass flow circulating in the secondary side of the HX, “*secondary*”;
- mass flow diverted by the mixer-diverter control, “*diverted*”, position 6’;

### 3.1.1. Energy evaluation

Table 10 shows the useful energy for each case.

*Table 10: useful energy in the 4 cases for the flat-level DHW preparation*

|                         | Case 1 | Case 2 | Case 3 | Case 4 |
|-------------------------|--------|--------|--------|--------|
| Useful energy [kWh/day] | 5.85   | 5.85   | 5.85   | 5.89   |

As it is possible to see, the daily amount of useful energy for DHW is achieved in each case, showing that the HX is well parametrized for these operative conditions.

## 3.1.2. Comfort

### Temperature development

The daily development of the temperatures can help to understand the influence of the DHW profile and of the logic of control on the behaviour of the HX. Figure 22 shows the temperatures development and the mass flows *primary*, *secondary* and *diverted* for case 1.

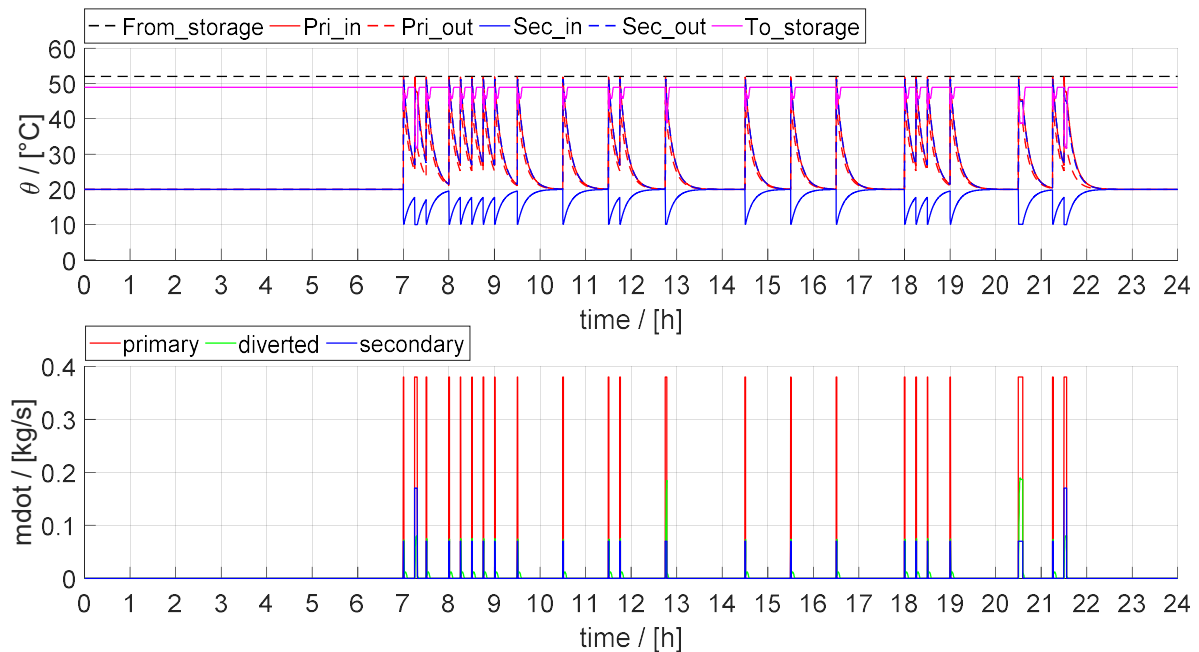


Figure 22: temperatures of the system and mass flow circulating in FWS in case 1 during one day

The temperature *From\_storage* of the water coming from the storage is fixed at 52°C. This water either circulates in the primary side of the HX or bypasses the HX when there is no request by the user.

In the period between 00:00 and 7:00, no mass flow enters the HX and so the temperature *Pri\_in* of the water entering the HX reaches the room temperature which is 20°C.

In order to have a more understandable representation of these trends, the period between 6:48 and 9:12 is shown in Figure 23. In this period a maximum load (due to the shower) and some small peaks occur.

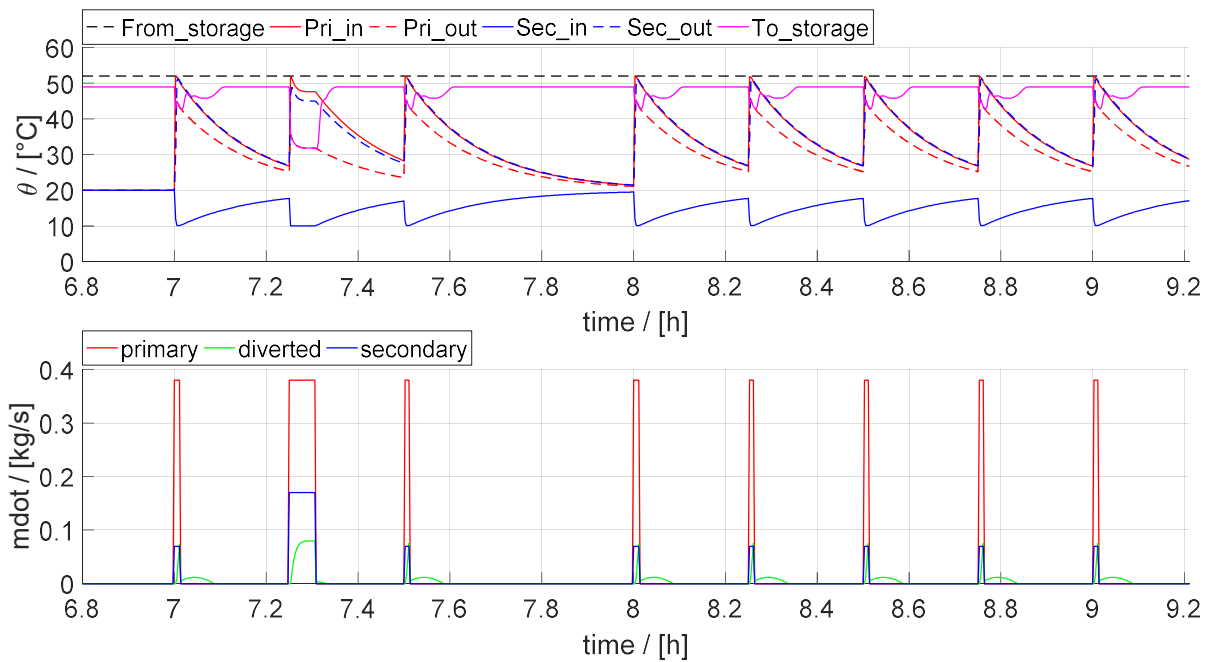


Figure 23: temperatures of the system and mass flow circulating in FWS in case 1 from 6:48 to 9:12

During the tapplings, the hot water from the storage enters the HX. The temperature of the water entering the HX in the primary side ( $Pri\_in$ ), changes from the temperature of the room to the temperature of the water coming from the storage. Once the tapping stops, this temperature decreases, reaching again the temperature of the room, with a delay due to the capacity of the HX.

When a tapping occurs, the mass flow circulating in the primary side of the HX is fixed at 0,38 kg/s. The higher the mass flow of the DHW supplied to the user, the lower the temperature of the water going out from the HX in the primary side ( $Pri\_out$ ).

For long periods without tapplings, the temperature of the water out of the HX in the secondary side ( $Sec\_out$ ) reaches the temperature of the room with a certain delay also due to the thermal capacity of the HX. As soon as a tapping starts, this temperature increases reaching a peak temperature that is higher than the set point, here fixed at 45°C. This is the reason why a user mixer-diverter control is needed. With a certain delay, the control stabilizes this temperature at the set point.

When the hot water bypasses the HX, it is reduced by the heat losses in the bypass pipe. In this case the temperature of the water sent back to the storage ( $To\_storage$ ) slightly differs from the temperature of the water coming from the storage ( $From\_storage$ ). When the hot water

circulates in the HX, instead, it is reduced by the heat exchanged with the cold water circulating in the secondary side. In this case it is desirable to have a lower temperature of the water sent back to the storage, in order to reduce the losses in the return pipe. The logic of the control used in each case, influences this temperature.

The same period between 6:48 and 9:12 is represented in Figure 24 for case 2.

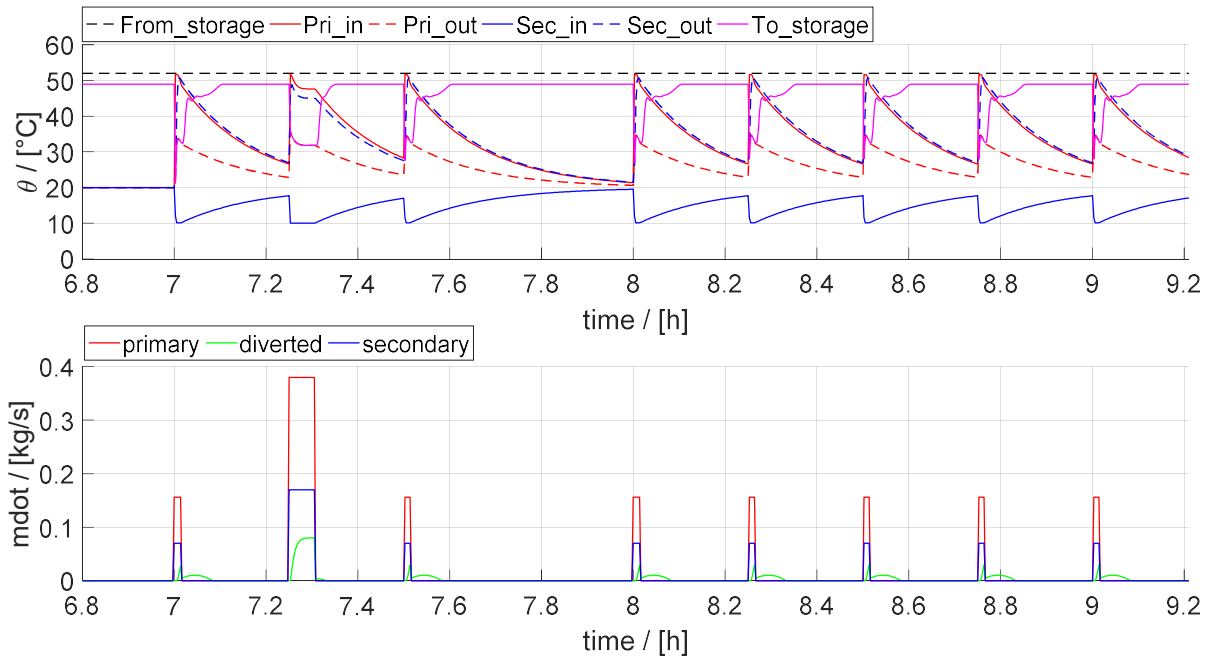


Figure 24: temperatures of the system and mass flow circulating in FWS in case 2 from 6:48 to 9:12

The discussion about the development of the temperatures for case 1 is still valid for case 2. The two cases differ on the mass flow circulating in the primary side of the HX (*primary*) that, in case 2, assumes different values according to the mass flow circulating in the secondary side (*secondary*). For the trend of the temperatures of the water coming from the storage, the water entering the HX in both the sides and the DHW supplied to the user (respectively: *From\_storage*, *Pri\_in*, *Sec\_in* and *Sec\_out*), no differences are observed in case 1 and case 2. The temperature development of the water leaving the HX in the primary side (*Pri\_out*) and of the water sent back to the storage (*To\_storage*), instead, is different for the two cases. For the first peak represented in Figure 23 and Figure 24, the mass flow circulating in the primary side of the HX (*primary*) is lower in case 2 than in case 1. It means that less energy is supplied to the HX during this peak and so that the temperature leaving the HX from the primary side (*Pri\_out*) is also lower in case 2 than in case 1. During the tapping, the temperature leaving the



HX from the primary side and the temperature of the water sent back to the storage are the same. This is also true for all the small tapplings occurring in the examined period. For the big tapping occurring at 7:15, the mass flow circulating in the primary side (*primary*) is the same in case 1 and case 2. Also the temperature leaving the HX from the primary side and the temperature of the water sent back to the storage are the same for the big tapping.

The comparison between the temperature of the water sent back to the storage (*To\_storage*) in case 1 and in case 2 is represented in Figure 25 in the period between 6:48 and 9:12.

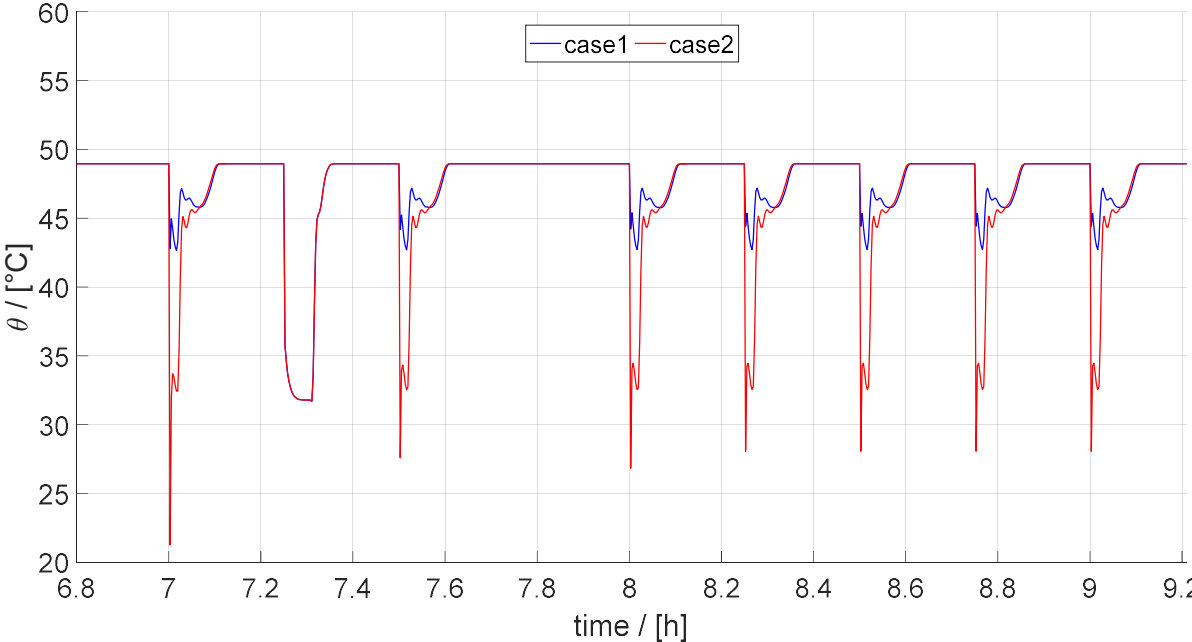


Figure 25: comparison of the temperature sent back to the storage for case 1 and case 2 in the period between 6:48 and 9:12

The comparison between the temperature of the DHW supplied to the user (*Sec\_out*) in case 1 and in case 2 is represented in Figure 26 in the period between 6:48 and 9:12.

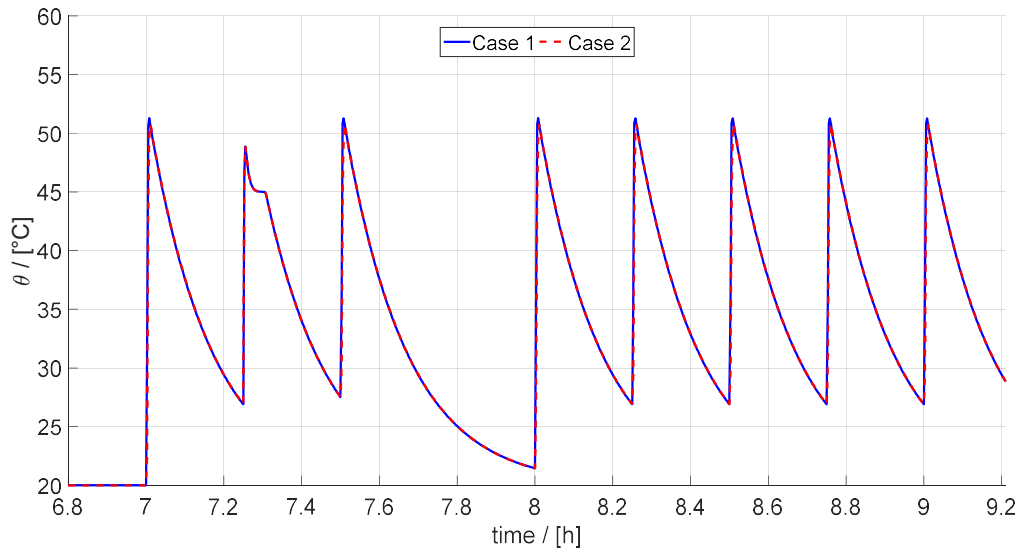


Figure 26: comparison between the temperature of the DHW supplied to the user for case 1 and case 2 in the period between 6:48 and 9:12

Figure 27 shows the temperatures development and the mass flows circulating in both the sides of the HX (*primary, secondary*) and the mass flow diverted by the mixer-diverter control (*diverted*) for case 3 during one day.

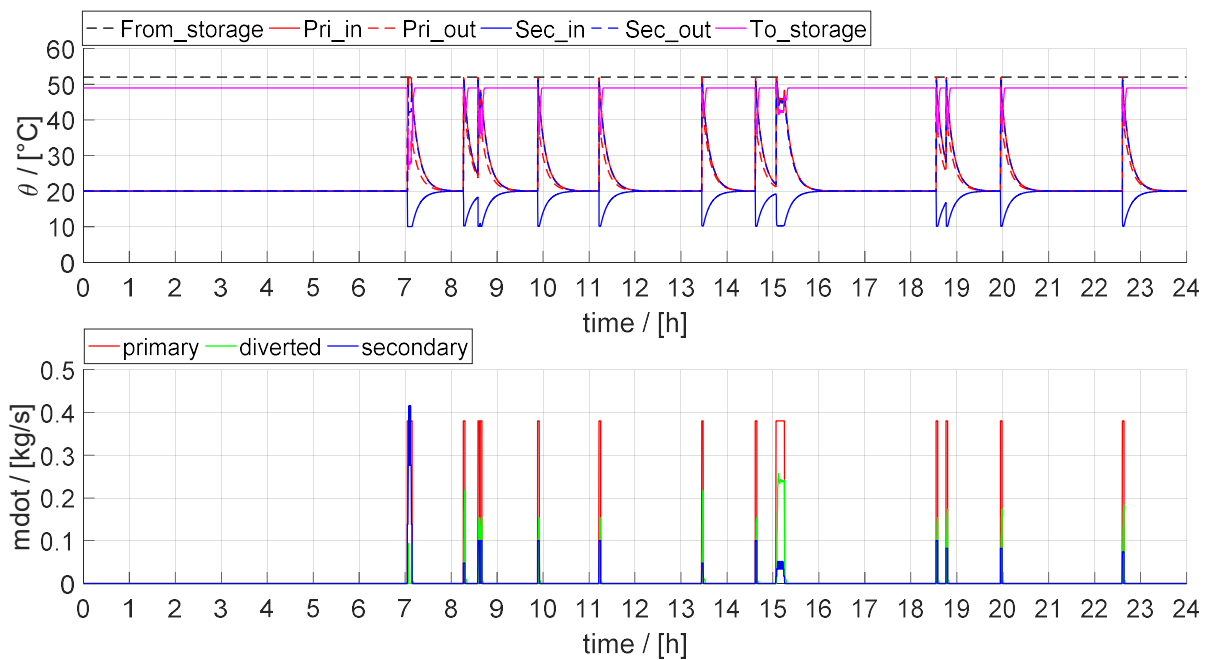


Figure 27: temperatures of the system and mass flow circulating in FWS in case 3 during one day

The considerations about the trend of the temperature of the water from the storage and of the water entering the storage in the primary side, made for case 1, are still valid for case 3. The temperature *From\_storage* of the water coming from the storage is fixed at 52°C: this water either circulates in the primary side of the HX or bypasses the HX when there is no request by the user.

In the period between 00:00 and 7:00, no mass flow enters the HX and so the temperature of the water entering the HX in the primary side (*Pri\_in*) reaches the room temperature which is 20°C.

Also in this case, the period between 6:48 and 9:12 is represented in Figure 28. In this period, a maximum peak occurs with a long tapping between 7:00 and 7:12, and two other lower tappings occur later on.

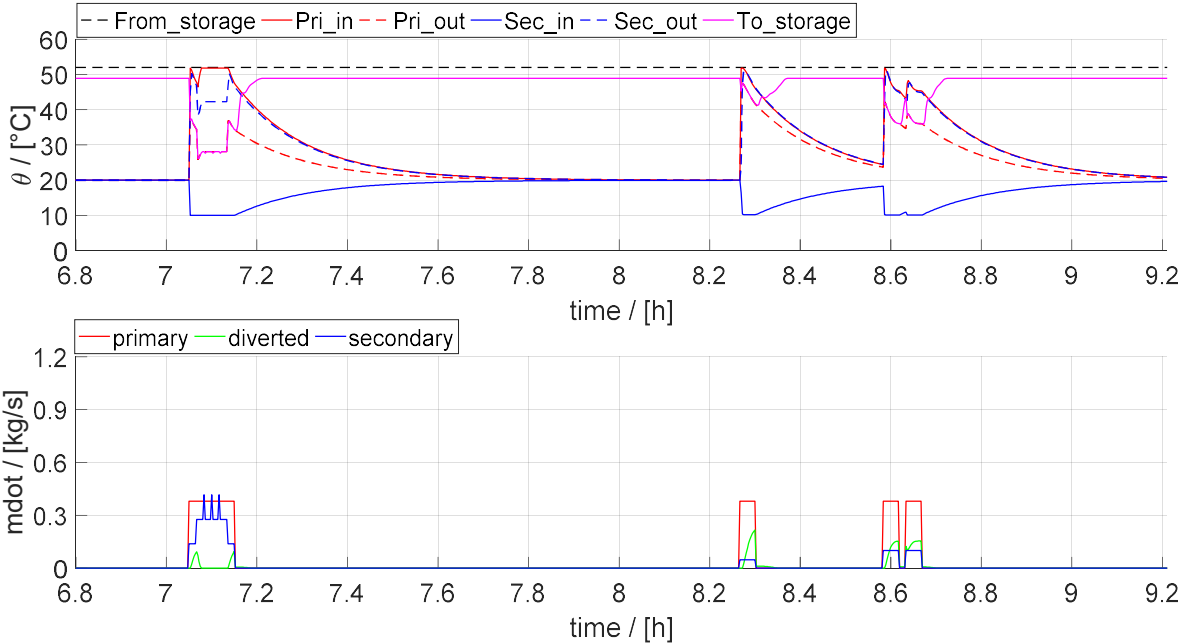


Figure 28: temperatures of the system and mass flow circulating in FWS in case 2 from 6:48 to 9:12

The mass flow *primary* circulating in the primary side, during the tappings, is always equal to 0,38 kg/s. In the first big tapping occurring in the morning, the mass flow *secondary*, circulating in the secondary side, changes throughout the duration of the tapping assuming values that are even higher than 0,38 kg/s. For this tapping, the temperature *Pri\_out* entering the HX, and so the temperature of the water sent back to the storage (*To\_storage*), reaches a value that is lower

than 30°C and this would be good in order to reduce the losses in the return pipe to the storage. However, the set point temperature of the DHW provided to the user (*Sec\_out*) is not achieved. This temperature reaches only 42°C.

The same period between 6:48 and 9:12 is represented in Figure 29 for case 4.

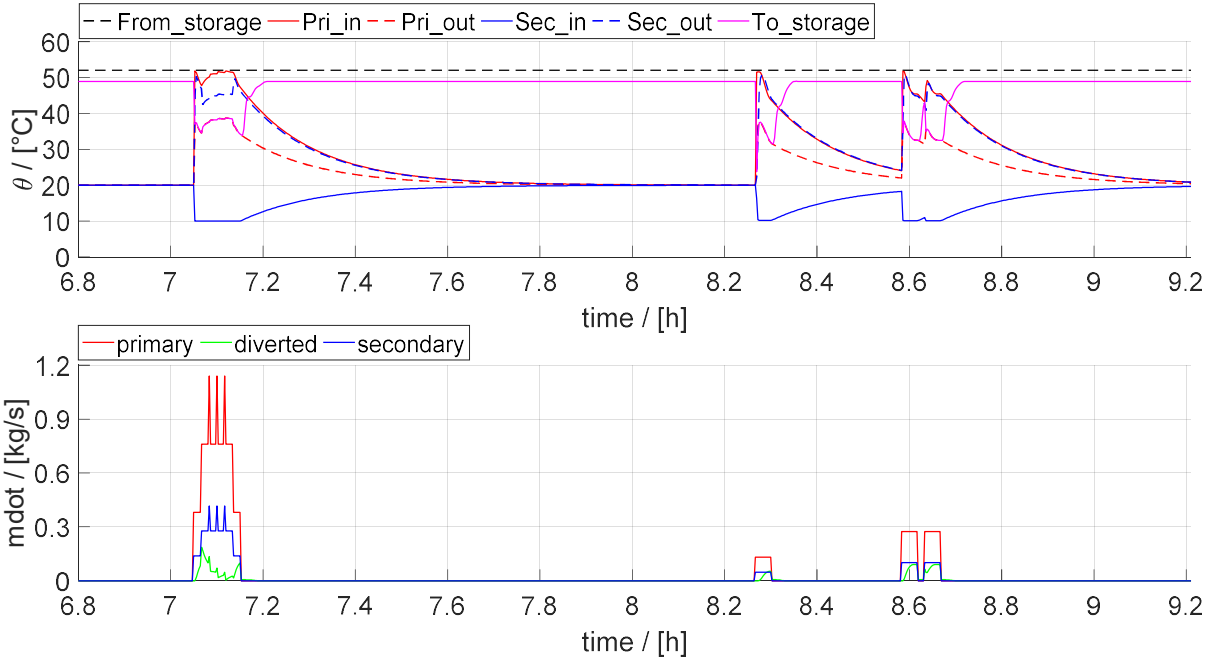


Figure 29: temperatures of the system and mass flow circulating in FWS in case 4 from 6:48 to 9:12

With a proportional control, the mass flow circulating in the primary side of the HX (*primary*) in the first tapping occurring in the morning in case 4 is higher than in case 3. During this tapping, in case 4, the set point of the DHW supplied to the user (*Sec\_ou*) (fixed at 45°C) is achieved. However, the temperature *Pri\_out* entering the HX in the primary side, and so the temperature *To\_storage* of the water sent back to the storage, during this tapping in case 4 are higher than in case 3. For the other three tapings represented in Figure 28 and Figure 29, the temperature *Pri\_out* and *To\_storage* in case 4 are lower than in case 3.

The comparison of the temperature *To\_storage* of the water sent back to the storage in case 3 and case 4 is presented in Figure 30 for the period between 6:48 and 9:12.

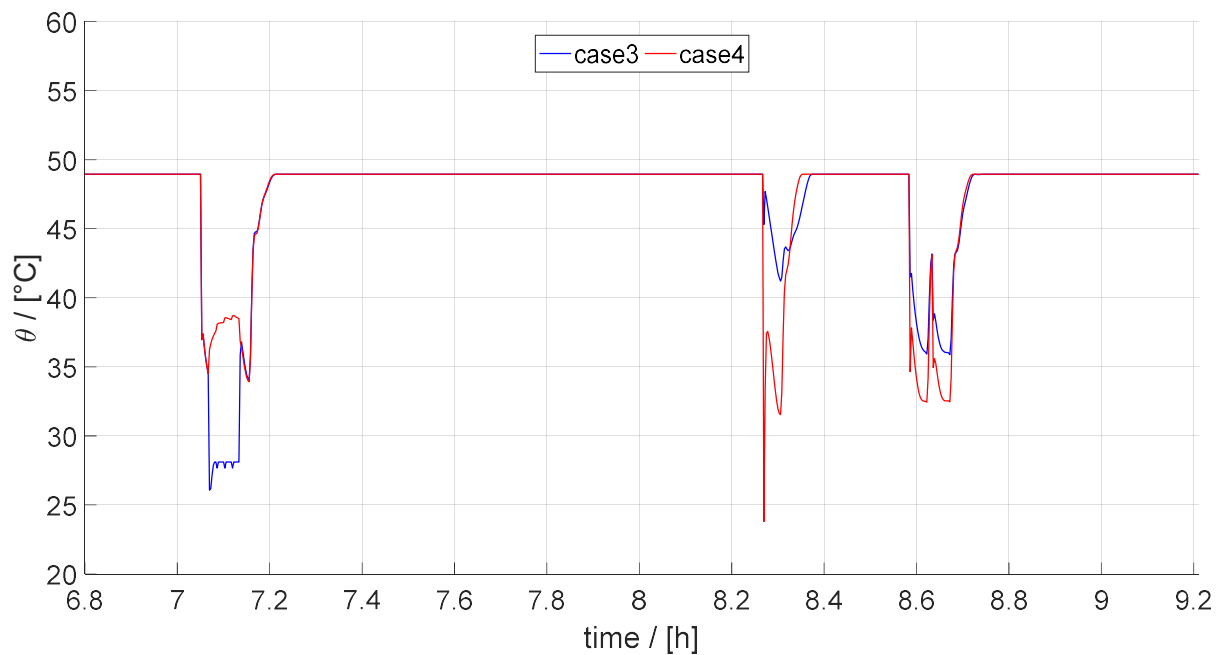


Figure 30: comparison of the temperature sent back to the storage for case 3 and case 4 in the period between 6:48 and 9:12

From the comparison between case 3 and case 4 it is possible to see that on-off control does not guarantee the set point temperature of the DHW supplied to the user ( $Sec\_out$ ) in the big tapping occurring in the morning for the stochastic profile derived from DHWcalc. Furthermore, for the small tappings spread all over the day, the proportional control allows to have a lower temperature of the water sent back to the storage.

The comparison between the temperature of the DHW supplied to the user ( $Sec\_out$ ) in case 3 and in case 4 is represented in Figure 31 in the period between 6:48 and 9:12.

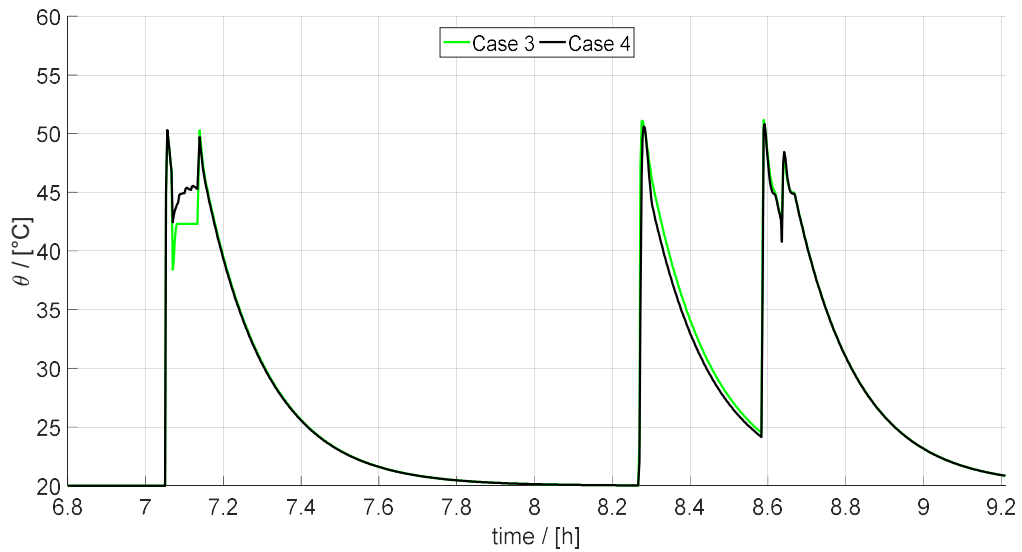


Figure 31: comparison between the temperature of the DHW supplied to the user for case 1 and case 2 in the period between 6:48 and 9:12

### Dynamic behaviour

The dynamic behaviour of the DHW supplied to the user is analysed focusing on selected tappings occurring in the period between 7:00 and 9:00. The “waiting time” is the time this temperature needs to reach at least the set point temperature, here fixed at 45°C.

For case 1, the small tapping occurring at 7:00, the waiting time is 19s. The comfort is fulfilled in 22s by reaching a peak temperature of 51°C. The same dynamic behaviour is also observed for the other small tappings occurring in the focused period. For the big tapping occurring at 07:15, the waiting time is 10s. Also for the big tapping, a peak temperature of 52°C is reached in 22s. As soon as the DHW temperature becomes higher than the set point, the mixer-diverter control works to stabilise the temperature to the set point and it works with a delay. For short tappings, the controller does not have enough time to stabilise the temperature on the set point. For longer tappings, like the one occurring at 7:15, from the peak temperature, the set point is reached in less than 70s.

For case 2, in the small tapping occurring at 7:00, the waiting time is 22 s. For the big tapping occurring at 7:15 the waiting time is 10s.

The waiting time for the tapping at 7:00 and for the one at 7:15 can be compared for case 1 and 2. Table 11 summarizes this comparison.

Table 11: waiting time of case 1 and case 2 for two tapplings occurring in the focused period

|        | Small tapping at 7:00 | Big tapping at 7:15 |
|--------|-----------------------|---------------------|
| Case 1 | 19 s                  | 10 s                |
| Case 2 | 22 s                  | 10 s                |

In Case 3 a big tapping occurs at 7:03. As already mentioned in the previous paragraph, for this tapping the set point temperature is not achieved. From the room temperature, the DHW temperature (*Sec\_out*) reaches the set point with a *waiting time* of 11s. Throughout this tapping, the mass flow *secondary* circulating in the secondary side, fluctuates and so does the temperature of the DHW for the first 100s. After these 100s, the DHW temperature is stabilised on a temperature equal to 42°C, lower than the set point. As already mentioned, for this tapping the comfort is not achieved. With the stochastic profile, at 8:15 a small tapping occurs. For this tapping the waiting time is equal to 17s. For the medium tapping occurring at 8:35, the waiting time is equal to 14s.

In case 4, for the big tapping occurring at 7:03, the waiting time is equal to 11s. 11s later, a peak temperature is reached. In this period, the mixer-diverter controller works to restore the set point temperature, slightly fluctuating around the set point for about 100s. For the small tapping occurring at 8:15, the waiting time is equal to 27s. For the medium tapping occurring at 8:35, the waiting time is equal to 17 s. Table 16 compares the waiting time of case 3 and case 4 for three tapplings occurring in the focused period.

Table 12: waiting time of case 3 and case 4 for three tapplings occurring in the focused period.

|        | Big tapping at 7:03 | Medium tapping at 8:35 | Small tapping at 8:15 |
|--------|---------------------|------------------------|-----------------------|
| Case 3 | No comfort          | 14 s                   | 17 s                  |
| Case 4 | 11 s                | 17 s                   | 27 s                  |

Regarding the dynamic behaviour of the DHW temperature supplied to the user (*Sec\_out*), no differences are observed for the big tapping occurring with the profile derived from standard EN16147 in case 1 and case 2. This means that for these big tapplings, the control does not influence the dynamic behaviour. For the small tapping, instead, a slightly bigger waiting time is observed in case 2. This means that the proportional control needs higher waiting time.

This is also observed from the comparison between case 3 and 4. The smaller the tapping, the higher the waiting time. In each tapping, case 3 has higher waiting time, confirming that the proportional control is slower reaching the set point temperature.

### 3.1.3. Discussion

As already mentioned, the required useful energy is achieved in each of the 4 cases. Independently from the DHW profile, the proportional control always assures the set point temperature of the DHW temperature (*Sec\_out*) and allows to have a lower temperature of the water sent back to the storage, in order to reduce the thermal losses in the return pipe. The on-off control does not allow to reach the set point temperature when the stochastic profile derived from DHWcalc is tested and this means that, with this control, the comfort is not guaranteed. From the comparison between the dynamic behaviours, it is possible to see that the proportional control gives a higher waiting time for both the profiles that have been tested. This higher waiting time is acceptable in order to guarantee the comfort in each tapping. The proportional control is more appropriate for such a simulation. This is the reason why this control is used for the building-level simulations.



## 3.2. Building-level results

Table 13 summarises the simulation cases for the flat-level DHW preparation.

*Table 13: simulation cases for building-level DHW preparation*

| BUILDING-LEVEL |                        |                     |
|----------------|------------------------|---------------------|
|                | Profile                | Size of the HX [kW] |
| Case 1         | Hourly average profile | 53                  |
| Case 2         | 10 s profile           | 280                 |
| Case 3         | 39 s profile           | 101                 |
| Case 4         | Stochastic profile     | 104                 |

According to Table 13, the DHW profile varies in the 4 cases. The parametrization of the HX gives different values for size, thermal capacity ( $C_{HX}$ ) and heat losses coefficient ( $UA_{HL}$ ).

Referring to Figure 6 the following temperatures are analysed:

- water from storage, “*From\_storage*”, position 9;
- water entering in the primary side of the HX, “*Pri\_in*”, position 11;
- water going out from the primary side of the HX, “*Pri\_out*”, position 12;
- water entering in the secondary side of the HX, “*Sec\_in*”, position 16;
- DHW temperature, “*Sec\_out*”, position 18;
- water entering the storage, “*To\_storage*”, position 14.

The trend of the mass flow circulating in the FWS is also analysed, referring to Figure 6:

- mass flow circulating in the primary side of the HX, “*primary*”;
- mass flow circulating in the secondary side of the HX, “*secondary*”;
- mass flow diverted by the mixer-diverter control, “*diverted*”, position 13’;

### 3.2.1. Energy evaluation

The energy supplied in different components for all the simulation cases is presented in Figure 32. The evaluation are focused on the following values of energy: energy from the DH (called “*final energy*”), energy supplied to the user (called “*useful energy*”), energy losses in the pipe

distribution system (called “*pipe distribution losses*”) and energy losses in the storage tank and in the storage charging circuit (called “*losses in technical room*”).

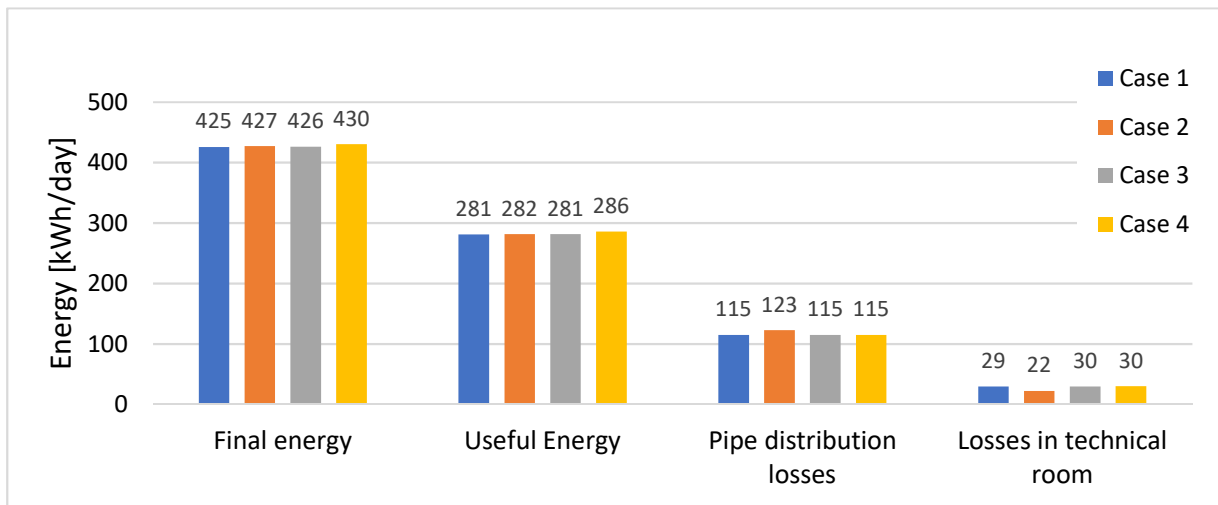


Figure 32: energy results from Building-level simulations.

The required *useful energy* is satisfied in all cases. For case 4 the useful energy is slightly higher due to the stochastic profile which shows a total DHW consumption, in this day, that is a bit higher than the daily consumption used in the other cases (the stochastic profile has the same daily average consumption of DHW but in a single day the consumption can be higher or lower than the average).

The same considerations can be made for the final energy from DH, where the highest value is registered for the case 4 while for the other cases the values are similar.

The highest losses occur in the pipes connecting the storage tank to the HX, so called “*pipe distribution losses*”. The higher value of these losses is observed for case 2 which has the highest return temperature to the storage. The value of the losses in the pipe distribution system for the three other cases are exactly the same. On the other hand, Case 2 shows lower values of the so-called *losses in technical room*, mainly because of the less losses occurring in the storage with this profile.

## 3.2.2. Comfort

### Temperature development

Figure 33 shows the temperatures development and the mass flows circulating in the primary and secondary side of the HX and the mass flow diverted by the mixer-diverter controller (respectively: *primary*, *secondary* and *diverted*) for case 1.

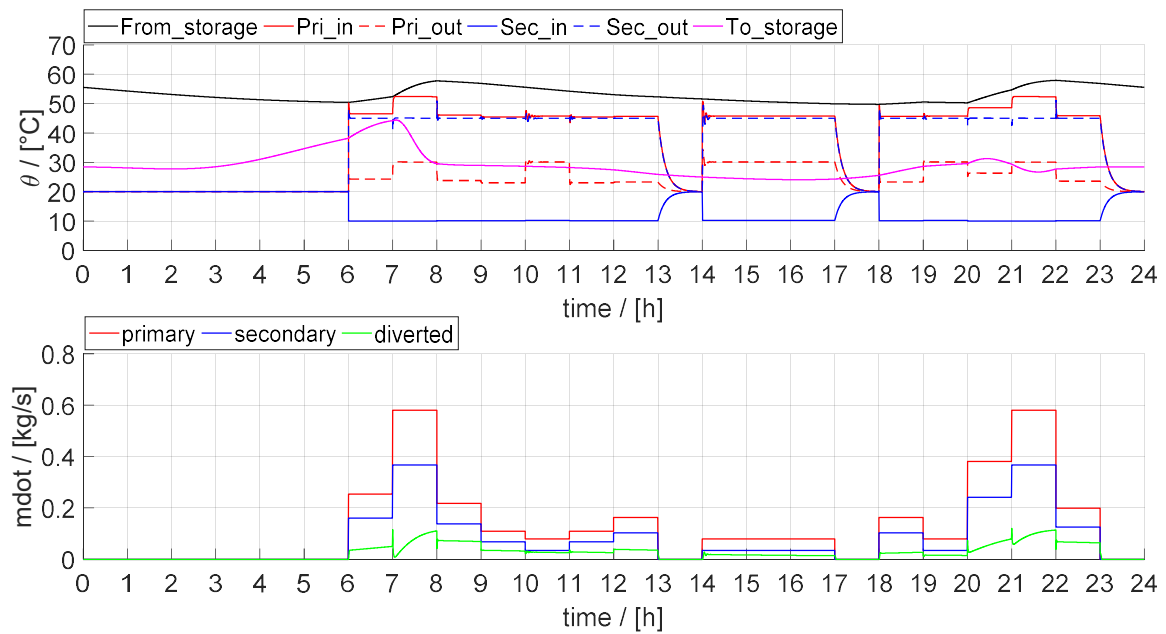


Figure 33: Temperatures of the system and mass flows circulating in FWS in case 1 during one day

First, the period between 00:00 and 6:00 is analysed. It is possible to observe that, in this period, the temperature of the water coming from the storage (*From\_storage*) decreases, while there is a minimum mass flow in the storage discharging circuit. In this period, the pipe wall loses the energy stored in the capacity during the operation time. While the minimum mass flow circulates in the pipe, this temperature decreases: the lower the capacity of the pipe, the faster the temperature drops.

The temperature *To\_storage* entering the storage presents an opposite behaviour. From 00:00 to 6:00, and so while there is no operation of the HX, the minimum mass flow circulates in this pipe. This is a hot water mass flow that bypasses the HX. In this period, this temperature increases with a certain delay due to the thermal capacity of the pipe. When the tapping starts, this temperature decreases. During the operation time of the HX, in fact, the mass flow in the

pipe back to the storage is the cold water after the exchange. The speed with which this temperature decreases, also depends on the capacity of the pipe.

When a long pipe is considered, the behaviour of the temperature *From\_storage* (coming from the storage) and *To\_storage* (entering the storage) explains the importance of the determination of the value of the capacity of the pipe. This value strongly influences the temperature development. These considerations explain the trend of the same temperatures also during the operation time of the heat exchanger.

The temperature *Sec\_out*, which is the temperature of the DHW provide to the user, reaches the room temperature when there is no request for DHW. As soon as the tappings start, this temperature reaches the set point. The set point temperature for the DHW (*Sec\_out*) is always reached during the tappings. The delay to reach the set point temperature is thoroughly analysed in the next paragraph.

For long periods with no operation, the cold temperature entering the heat exchanger in the secondary side (*Sec\_in*) reaches the room temperature. As soon as the tappings start, this temperature reaches instantaneously the temperature of the cold water (here considered equal to 10°C). When the tappings stop, this temperature rises again to the room temperature with a certain delay due to the capacity of the heat exchanger.

The temperature *Pri\_in* is the temperature of the water entering the heat exchanger. While there is no operation of the HX, this temperature reaches the value of the room temperature. During the operation time of the HX, the temperature *Pri\_in* is controlled by the mixer-diverter controller in order to assure a hot source for the HX that guarantees the set point temperature of the DHW (*Sec\_out*). The higher the temperature *From\_storage* coming from the storage, the higher the mass flow diverted by the mixer-diverter control (*diverter* in Figure 33).

The temperature *Pri\_out* is the temperature of the water going out from the primary side of the HX. During the no-operation periods of the HX, this temperature reaches the room temperature. During the operation period of the HX, instead, this temperature depends on the heat exchanged with the mass flow circulating in the secondary side of the HX.

This discussion also explains the trends of these temperatures for the three other cases. The trends of these temperatures for case 2, case 3 and case 4 are shown in Figure 34, Figure 35, Figure 36.

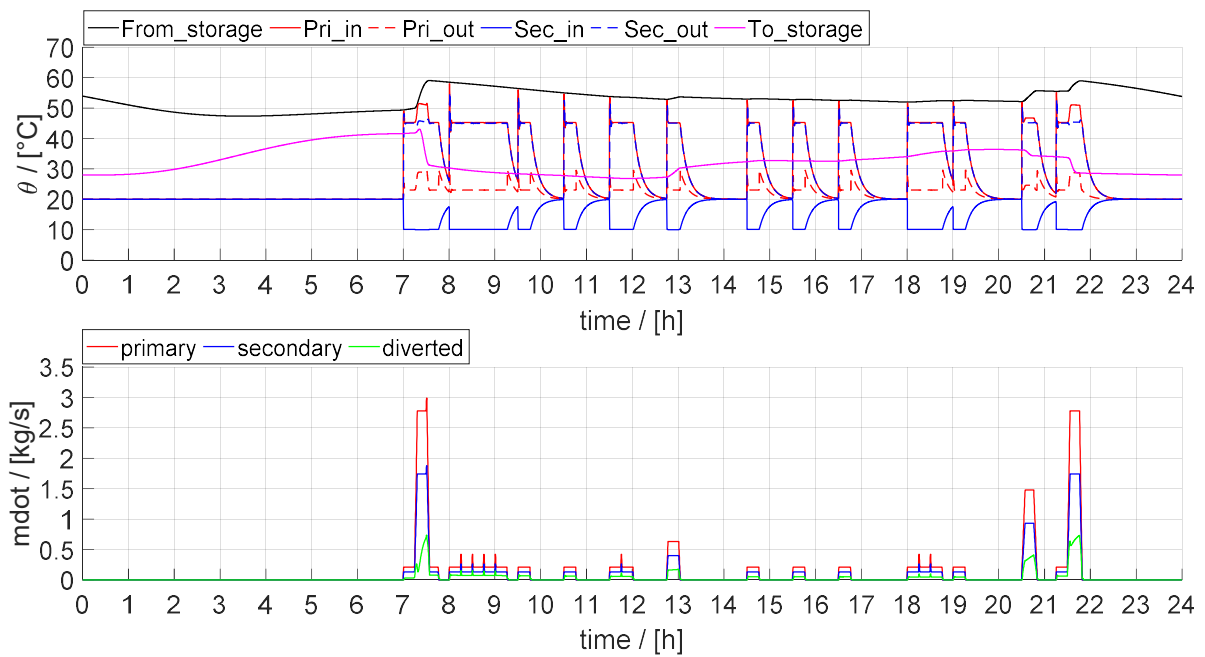


Figure 34: Temperatures of the system and mass flows circulating in FWS in case 2 during one day

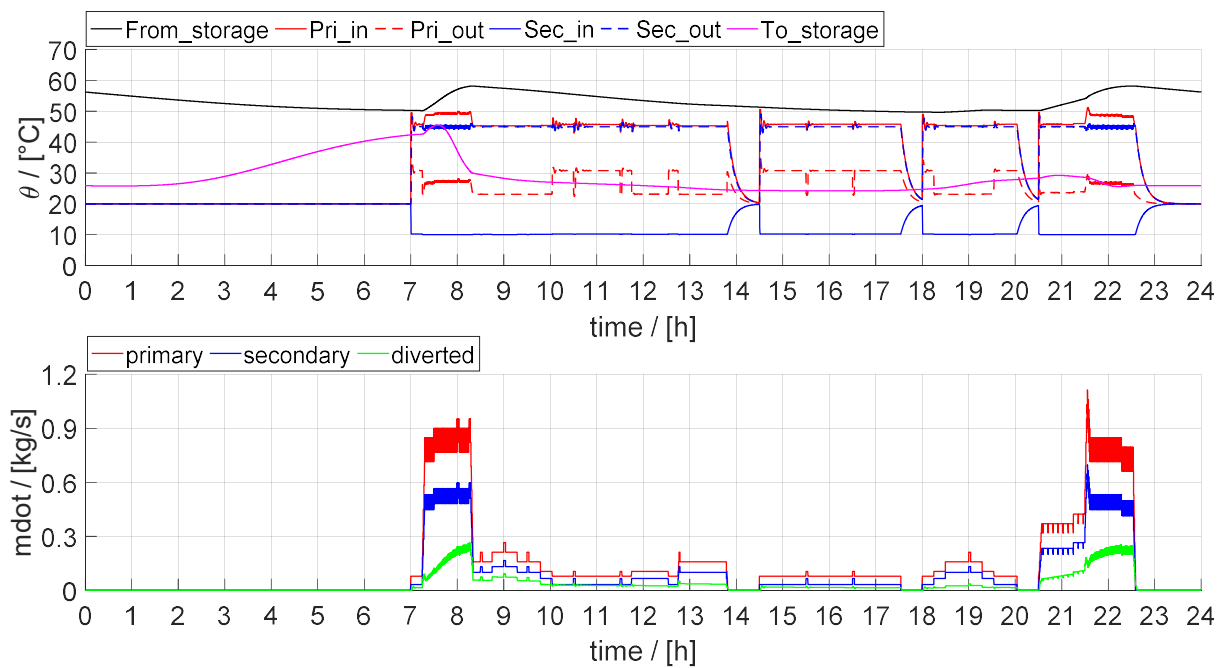
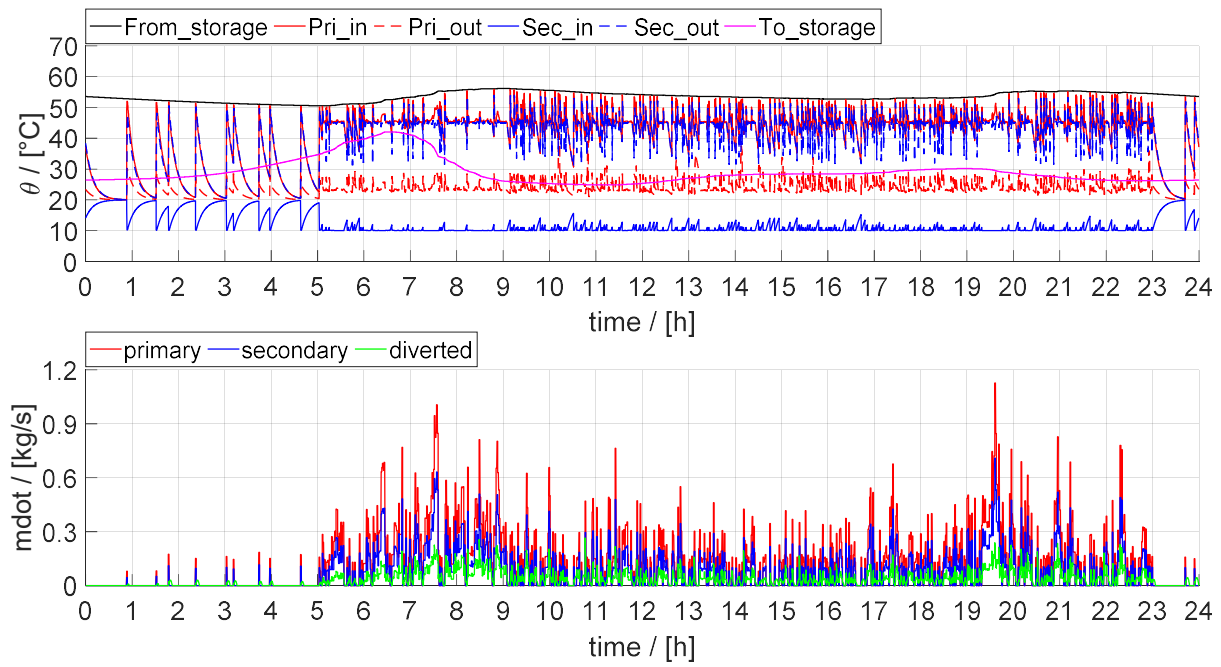


Figure 35: Temperatures of the system and mass flows circulating in FWS in case 3 during one day



*Figure 36: Temperatures of the system and mass flows circulating in FWS in case 4 during one day*

Thus, from the simulation is shown that, with a 426 m pipe, the capacity of the pipes always plays a big role in the determination of the temperatures.

The temperature  $To_{storage}$  of the water reaching the storage from the HX plays a big role on the heat losses of the system. It is interesting to compare the trend of this temperature in the four simulated cases. Figure 37 shows the trends of this temperature in the four analysed cases also referring to the DHW profiles.

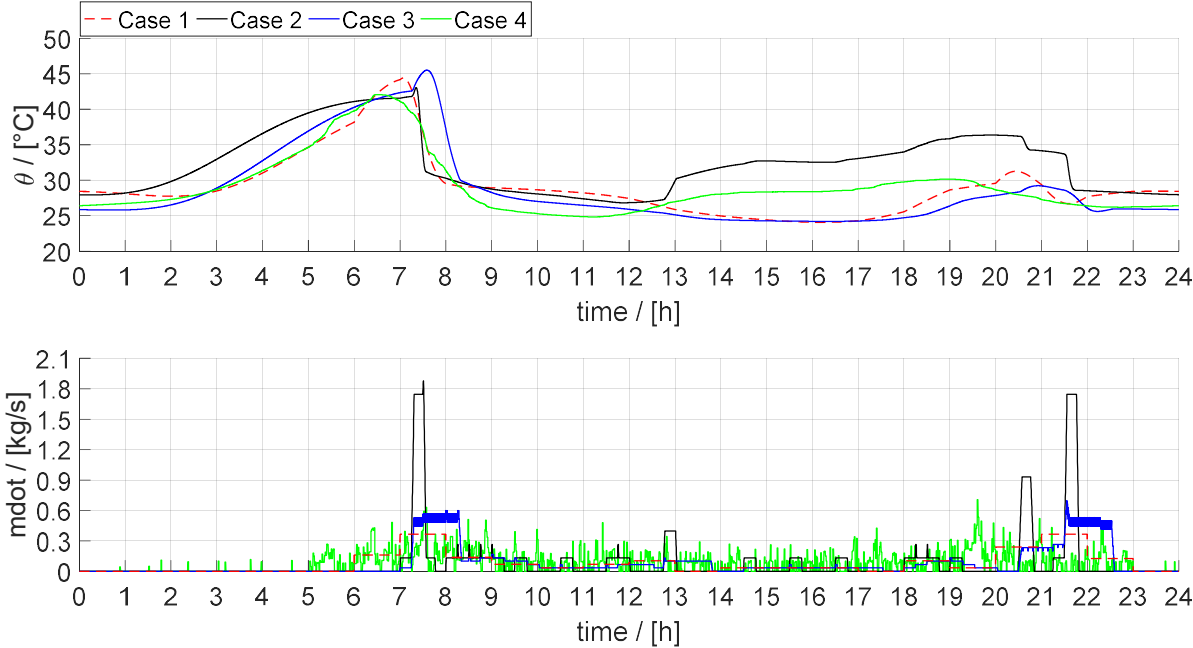


Figure 37: Return temperature to the storage and DHW profiles in the 4 analysed cases

For all the cases, the temperatures show the same trend in the period between 00:00 and 6:00. In this period no tappings occur considering case 1, case 2 and case 3, while only small and short tappings occur in case 4. The small tappings occurring in case 4 during this period, do not influence so much the rise of the temperature. In the period between 7:00 and 8:00 all the temperature drops in all the 4 cases. In this period, in fact, peak loads (due to the showers) occur for all the cases. For case 2, which has the biggest peak load after 7:15, the temperature drop is the fastest.

In the period between 13:00 and 21:00 the trends deviate. For case 2 and case 4, the temperature is significantly higher if compared to case 1 and case 3. In this period, case 2 and case 4 present a more intermittent DHW profile and so more intermittent HX operation. Case 1 and case 3, instead, present a more stable profile, with HX operation all over the period. It means that for profiles with intermittent request, this temperature is always kept higher if compared to profiles with a more stable request spread all over the period. The tested DHW profile strongly influences the development of this temperature.

For this temperature, Table 14 shows the mean hourly value and the minimum hourly value.

*Table 14: mean hourly temperature and minimum hourly temperature of the water back to the storage in °C*

|    | Case 1 |     | Case 2 |     | Case 3 |     | Case 4 |     |
|----|--------|-----|--------|-----|--------|-----|--------|-----|
|    | mean   | min | mean   | min | mean   | min | mean   | min |
| 1  | 28     | 28  | 28     | 28  | 26     | 26  | 27     | 26  |
| 2  | 28     | 28  | 29     | 28  | 26     | 26  | 27     | 27  |
| 3  | 28     | 28  | 31     | 30  | 28     | 27  | 28     | 27  |
| 4  | 30     | 28  | 35     | 33  | 31     | 29  | 30     | 29  |
| 5  | 33     | 31  | 38     | 37  | 35     | 33  | 33     | 31  |
| 6  | 36     | 35  | 40     | 39  | 39     | 37  | 38     | 35  |
| 7  | 42     | 38  | 41     | 41  | 41     | 40  | 41     | 40  |
| 8  | 37     | 30  | 36     | 30  | 43     | 37  | 36     | 31  |
| 9  | 29     | 29  | 29     | 29  | 30     | 28  | 28     | 26  |
| 10 | 29     | 29  | 28     | 28  | 28     | 27  | 26     | 25  |
| 11 | 28     | 28  | 28     | 27  | 27     | 26  | 25     | 25  |
| 12 | 28     | 27  | 27     | 27  | 26     | 26  | 25     | 25  |
| 13 | 27     | 26  | 27     | 27  | 26     | 25  | 26     | 25  |
| 14 | 25     | 25  | 31     | 30  | 25     | 24  | 28     | 27  |
| 15 | 25     | 24  | 32     | 32  | 24     | 24  | 28     | 28  |
| 16 | 24     | 24  | 33     | 33  | 24     | 24  | 28     | 28  |
| 17 | 24     | 24  | 33     | 33  | 24     | 24  | 29     | 28  |
| 18 | 25     | 24  | 34     | 33  | 24     | 24  | 29     | 29  |
| 19 | 27     | 26  | 35     | 34  | 25     | 25  | 30     | 30  |
| 20 | 29     | 29  | 36     | 36  | 27     | 26  | 30     | 29  |
| 21 | 31     | 29  | 36     | 34  | 29     | 28  | 28     | 27  |
| 22 | 27     | 27  | 32     | 29  | 28     | 26  | 27     | 26  |
| 23 | 28     | 28  | 28     | 28  | 26     | 26  | 26     | 26  |
| 24 | 28     | 28  | 28     | 28  | 26     | 26  | 26     | 26  |

The tested DHW profile strongly influences the development of this temperature. This temperature is very important when a DHW preparation with HP is considered.



## Dynamic behaviour

The dynamic behaviour of the DHW temperature supplied to the user is analysed. The “*waiting time*” is the time needed to reach at least the set point temperature of the water provided to the user, here fixed at 45°C. This time strongly depends on the mass flow of the tapplings and the duration of the tapplings. The control of the mixer-diverter that aims to stabilize the temperature at the set point can cause fluctuations around this set point.

In Case 1, the tapplings start at 6:00 and the value of the mass flow is kept constant for one hour and it is equal to 0,16 kg/s. The waiting time of the DHW to reach the set point, starting from the room temperature, is 20s. Then the temperature is stabilized by the mixer-diverter controller with no other fluctuations around the set point. Variations on the mass flow supplied to the user cause small fluctuations which are extinguished in less than 90 s.

In Case 2 the first tapplings in the morning start at 7:00 with a mass flow that increases from 0 kg/s to 0.13 kg/s in 29s. The *waiting time* of the DHW to reach the set point, starting from the room temperature, is 44s, then the temperature is stabilized to the set point. Small fluctuations of 1 K around the set point occur when the mass flow increases. In comparison with Case 1, the longer time is due to the lower mass flow request during the first seconds of the tapplings.

In Case 3 the morning tapplings also start at 7:00 and a constant mass flow of 0.03 kg/s is kept constant for 15 minutes. The *waiting time* of the DHW to reach the set point, starting from the room temperature, is 68s. In comparison with Case 2, a small mass flow is kept for a longer time, this is the reason why the delay time to reach the set point is higher, then the temperature is stabilised on the set point. From 7:18, the DHW mass flow request begins to rapidly fluctuate, causing a small fluctuation also in the DHW temperature. The fluctuations of about 0.5 K around the set point are not even appreciable and prove the control responds to the perturbations.

In Case 4 the tapplings are spread all over the day. In regarding to a small isolated tapping occurring at 00:53, the *waiting time* is 50s. For a longer lasting tapping occurring at 5:02, the set point temperature is reached in 28 s. During the day, continuous tapplings occur and the analysed temperature has no time to reach the room temperature. For this reason, in case 4, this temperature always fluctuates around the set point temperature.

The *waiting time* for the tapplings occurring in the morning for case 1, case 2 and case 3 are shown in Table 15; two values are shown for case 4: the small isolated tapping occurring during the night and the morning tapping at 5:02 which is the first tapping occurring in the morning in which the DHW is heated up starting from the room temperature.

Table 15: waiting time to reach the set point temperature in the morning tapping for case 1, case 2 and case 3 and for two tappings in case 4.

|                  | Case 1 | Case 2 | Case 3 | Case 4                 |                     |
|------------------|--------|--------|--------|------------------------|---------------------|
|                  |        |        |        | small isolated tapping | big tapping at 5:02 |
| Waiting time [s] | 20     | 44     | 68     | 50                     | 28                  |

The chosen profile strongly influences the dynamic of the variation of the temperatures in the HX. The more irregular the profile, the higher the fluctuations of the temperature of the DHW supplied to the user. Stable temperatures are obtained for long lasting tappings with high mass flow. For the analysed tappings it is observed that the highest the DHW request, the shorter the *waiting time*.

# Chapter 4. Comparison between one HX per flat and one HX for the whole building

A method to simulate the DHW preparation for a big multi-family building has been developed. In order to test this method, a comparison between the physical model with one HX per each flat and the model with one HX for the whole building (building-level HX) is made. A smaller multi-family building is considered to make this comparison possible. Useful energy for DHW and pipe losses are analysed in the comparison.

## 4.1. Concept

The reference building is a 10-flat building taken from the study by Samuel Breuss who developed the model for heating system and DHW preparation. The hydraulic scheme of the system is shown in Figure 38.

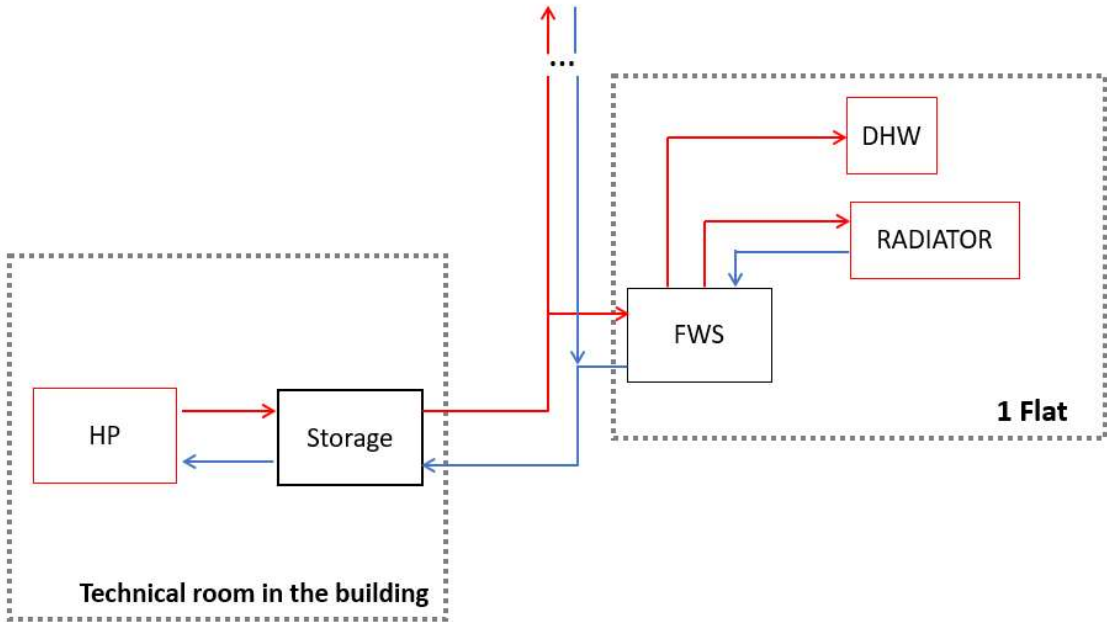


Figure 38: hydraulic scheme of the 2-pipe system for a 10-flat building.

The pipe distribution system for this study is a 2-pipe system with FWS in each flat for combined space heating with radiators and DHW preparation. The hot source for the FWS comes from the storage placed in the technical room of the building. The storage is heated up by a HP. The comparison only takes into account the DHW preparation. The hydraulic distribution system is shown in Figure 39.

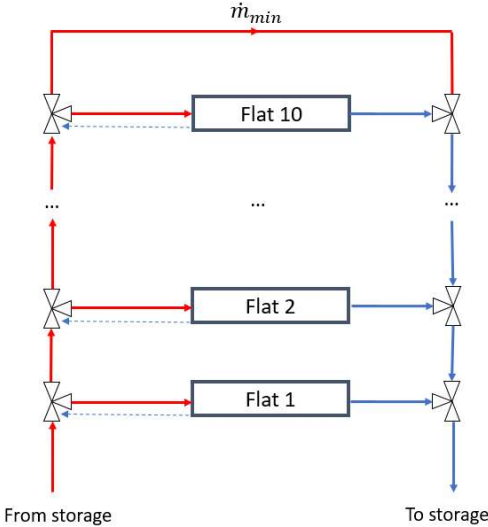


Figure 39: Hydraulic distribution system for the 10-flat building.

The subsystem in each flat is shown in Figure 40.

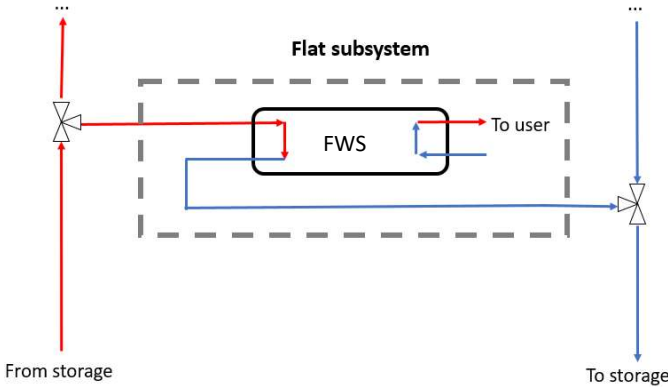


Figure 40: DHW preparation subsystem in each flat

## 4.2. Simulation model and DHW profiles

In regarding to the space heating, this is simulated as a single thermal zone including 10 flats. However, the results regarding the space heating are not analysed. For the DHW preparation, instead, two different approaches are considered. In the first approach one FWS for each flat is modelled (physical approach). In the second approach, instead, one HX for the whole building is modelled (building-level DHW preparation). Useful energy for DHW and pipe losses are evaluated from both approaches.

For the proper modelling of the FWS, DHW profiles should be derived. 10 different stochastic profiles are derived from DHWcalc, one per each flat. For the model with a single heat exchanger for the whole building, the 10 profiles are summed. For the model with one heat exchanger for each flat, the profiles are implemented in two different ways: in the “*star configuration model*” each of the 10 profiles is implemented in a different flat; in the “*star configuration shifted*”, instead, one of the 10 profiles is chosen and it is implemented in each flat, choosing a delay of 300s on the starting time of the daily tapping cycles. For the different profiles, a different values of simultaneity factor is considered in order to parametrise the building-level HX.

## 4.3. Comparison results

The results from two different simulations models are analysed: the model with one HX for the whole building and the model with 1 HX per each flat (which is considered with two different implementations of the DHW profiles). Results regarding useful energy for DHW preparation and pipe thermal losses are compared in the three different one-year simulations and they are shown in Table 16.

*Table 16: results from the comparison between the implemented models*

|   | 1 HX for the<br>whole building | 1 HX for each flat |                            |
|---|--------------------------------|--------------------|----------------------------|
|   |                                | Star configuration | Star configuration shifted |
| Useful energy<br>[kWh/(m <sup>2</sup> ·year)]       | 21.74                          | 21.74              | 21.72                      |
| Pipe thermal losses<br>[kWh/(m <sup>2</sup> ·year)] | 1.32                           | 1.16               | 1.22                       |

With respect to the useful energy, no difference is observed in the three models. For the pipe thermal losses, an appreciable difference is observed between the models. An optimistic insulation level is considered for the pipes. This is the reason why the pipe thermal losses are very low respect to the useful energy. The insulation level is optimistic but, in reality, a less performant insulation is used. For the insulation level considered in the study, the thermal pipe losses for the model with the building-level HX are higher than the values for the model with one HX for each flat, in both the configurations (*star configuration* and *star configuration shifted*). However, this difference is into an acceptable range: for the *star configuration* it is 12% higher, while for the *star configuration shifted* it results to be 8% higher. Future studies will analyse the effect of the insulation of the pipe in the results. In order to evaluate the influence of the insulation on the results, further studies will be made.

With the boundaries and the conditions considered in this study, the implemented method with a HX is reliable to make consideration on useful energy and pipe thermal losses. Similar considerations will be made on the dynamic behaviour of the systems and the comfort for the user, in order to evaluate the comparison between the two approaches.

# Chapter 5. Conclusions

In this master thesis, a modelling method for DHW preparation for big multi-family buildings has been developed in order to evaluate and optimize the final energy and the DHW comfort (measured as supplied temperature to the user and the so-called waiting time to reach this temperature). The case study is a multi-family building composed by 96 flats placed in the new residential district “Campagne” that will be built in Innsbruck. District heating (DH) is used to heat up the DHW storage, which is located in the technical room of the building. The storage is connected to all the flats through a distribution system. In each flat, a fresh water station (FWS) is located for the DHW preparation.

Different DHW profiles are generated and simulations are performed in order to investigate the influence of these profiles. The daily DHW profiles are derived either from standard profiles, e.g. EN16147 (here, profile M) or from tool, e.g. *DHWcalc* which creates a DHW profile using a stochastic approach.

Three different approaches can be considered for the simulation on building-level. The physical approach is to simulate the whole building with one heat exchanger (HX) in each flat; the second approach is to simulate the flat and extrapolate the results to the building ; the third approach is to simulate the whole building with one single HX sized considering the simultaneity factor, i.e. considering that only a limited number of flats will consume DHW at the same time. For such a big multi-family building, the physical approach would lead to a very heavy model with extensive simulation times and high computational effort, for this reason, this approach is not considered to be feasible. The second leads to a significant overestimation of the required heating power. The peak loads of each flat, in fact, never occur simultaneously. Hence, the third approach is chosen as the most appropriate for the simulations in the framework of this thesis. However, in addition, the physical approach of one HX for each flat and the approach of one HX for the whole building are compared using a small multi-family building composed of 10 flats. With respect to the useful energy, the results show that the value for the physical model is the same of the model with one HX for the whole building. With respect to the pipe losses, the value for the model with one single HX for the whole building is higher than the value for the physical model with one HX per each flat (varying between 7,5% and 12%, depending on the tested profiles), but still within an acceptable range for the considered level of pipe insulation.

First, a model of a flat-level DHW preparation system is implemented in Matlab/Simulink simulation environment considering a 35-kW HX, (size of the HX of a typical market available fresh water station). Two different DHW profiles (from standard EN16147 profile M, and stochastic profile) are tested together with two different control strategies of the circulation pump of the primary side of the HX (on-off and proportional). The results show that the required useful energy is achieved in each of the simulated cases. The proportional control always assures the set point temperature of the DHW provided to the user, independently from the tested DHW profile, even with a slightly longer waiting time. The proportional control also allows to have lower temperature of the water coming out from the primary side of the HX and this is beneficial in order to reduce the thermal losses of the return pipe to the storage. The proportional control is chosen as the most appropriate and it is further used in the building-level model.

A model of a building-level DHW preparation system is then derived from the flat-level model, in order to make consideration about thermal losses in the distribution system and about the return temperature to the storage (i.e. influence on thermal losses and final energy). From the flat-level DHW profiles, four different profiles are derived for the building-level. Each of the four profiles has a different peak load and thus, a different simultaneity factor. The HX is sized based on the peak DHW load of the building. The most relevant parameters are the heat transfer coefficient between primary and secondary side ( $UA_{HX}$ ), the heat transfer coefficient to the ambient ( $UA_{HL}$ ) and thermal capacity ( $C_{HX}$ ) of the HX and they are calculated for each case. For each case, first it is controlled that the required useful energy is achieved. The different tested profiles influence the development of the return temperature to the storage. This temperature is also influenced by the thermal capacity of the return pipe to the storage. For the *10s profile* (which is the one with the highest simultaneity factor), the return temperature to the storage has highest values in the period between 13:00 and 22:00, if compared to the other tested profiles. This is the reason why the thermal losses observed in this case are slightly higher than the thermal losses of the other cases. The DHW profile, for the building-level simulations, strongly influences the waiting time which is longer for lower loads and shorter for the peak loads.

Future studies should investigate the influence of different boundary conditions and DHW system design, such as different logics of control for the building-level DHW preparation or different set point temperature for the DHW supply. It is further necessary to investigate the influence of different thermal insulation levels of the pipes on the development of the return



temperature to the storage and the thermal losses. The study of the return temperature is relevant with different DHW preparation systems in particular in case of heat pumps, where the return temperature has significant influence on the system performance.

# Acknowledgment

Now more than ever I feel so excited to live what the future holds for me. I am ready to face it putting into practice all the teachings that I got from the people I met along these years. Working on this master thesis, in particular, I got the chance to meet people of big value who shared their knowledge with me.

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